To all our customers,

We are pleased to share with you our most recent Technology Handbook. It provides a comprehensive overview of our portfolio of advanced technologies – some 64 of them, each designed to provide sustainable solutions to your business.

Our ambition is to be the partner of choice for the design, engineering and construction of state-of-the-art production units worldwide. We work continuously to increase the value of our technologies and expand our knowledge to serve our customers better. Innovation is vital, and our internal technology experts and research networks work closely with our development teams and plant operators to develop ideas and new approaches that meet our clients’ needs. We stay close to the markets and customers we serve, allowing us to develop our technological leadership for our customers’ benefit.

A fundamental goal at Air Liquide Engineering & Construction is to provide our customers with competitive solutions that are safe and reliable. Our aim is to make sure that our customers can secure the best possible performance from their operations and make the most efficient use of natural resources.

We encourage you to contact us through our regional offices or one of our technology groups. Our experts and project leaders will be at your disposal and ready to offer additional information to help your business grow and prosper.

Value through technology

Domenico D’Elia
Senior Vice President Sales and Technology
Air Liquide Engineering & Construction
Air Liquide

The world leader in gases, technologies and services for Industry and Health

We are present in 80 countries with approximately 65,000 employees, serving more than 3.5 million customers and patients.

Oxygen, nitrogen and hydrogen have been at the core of the company’s activities since its creation in 1902. They are essential small molecules for life, matter and energy. They embody Air Liquide’s scientific territory.

Air Liquide’s ambition is to lead its industry, deliver long-term performance and contribute to sustainability. The company’s customer-centric transformation strategy aims to achieve profitable growth for the long term. It relies on operational excellence, selective investments, open innovation and a network organization implemented by the Group worldwide. Through the commitment and inventiveness of its people, Air Liquide is helping to deliver a transition in energy and the environment, provide changes in healthcare and digitization, and deliver greater value to all its stakeholders.
Air Liquide Engineering & Construction

A technology partner of choice

Air Liquide Engineering & Construction, the engineering and construction business of the Air Liquide Group, builds the Group’s production units – mainly air gas separation and hydrogen production units – and supplies external customers with its portfolio of technologies. Its industrial gas, energy conversion and gas purification technologies enable customers to optimize the use of natural resources.

We cover the entire project life-cycle: from license engineering services / proprietary equipment, high-end engineering and design capabilities, as well as project management, commissioning and execution. Its exclusive and innovative technologies are contributing to the transition of the energy sector.

With more than 1,600 patents we are at work, connecting people and ideas everywhere to create advanced technologies to solve customer issues.
Inventiveness, open-mindedness, sharing, agility and entrepreneurial mindset are fundamental features of our innovation approach.

Our Group innovation network is built on science, technologies, and dedicated investments. It is focused on developing new approaches and services for customers and patients, accelerated by digital transformation. It is part of an open ecosystem in which advances are rapidly shared across Air Liquide and with our external scientific partners and start-ups.

Innovation improves our customers’ experience, contributes to growth and to the creation of a more sustainable world.

We innovate across all our areas of activity, balancing its drive for innovation with a commitment to preserve and maintain core products. By combining this pragmatic approach with technical creativity, our teams deliver unique solutions that make a real difference to our customers. Here are just a few examples of recent innovations.
Innovation in action

**Cryocap™, CO₂ cold capture system**
Cryocap™ enables the capture of CO₂ released during hydrogen production via a cryogenic process. The first industrial deployment of this technology was made in Port-Jérôme, France, at the largest steam methane reforming hydrogen production unit operated by Air Liquide.

**Cryogenic Technology Center**
At our Cryogenic Technology Center in Vitry-sur-Seine, France, innovations related to cryogenic technology topics are developed, tested and demonstrated in an accelerated innovation cycle, thus being ready for early industrialization.

**SMR-X, a zero steam hydrogen plant solution**
SMR-X enables zero steam hydrogen production, with 4% natural gas fuel savings and 4% reduced CO₂ emissions compared to conventional installations.

**A full portfolio of solutions for the LNG market**
We offer customers a suite of highly efficient and proven LNG technologies based on our own proprietary processes using plate fin heat exchangers technology.

**World’s largest plants for industrial gas production**
We have designed and assembled the largest single train air separation unit ever built. With a total capacity of 5,800 tons of oxygen per day (at mean sea level), the unit will supply industrial gases to the Secunda site for Sasol in South Africa. We have also designed and built units for the global-scale hydrogen production site in Yanbu Industrial City in Saudi Arabia with a total capacity of 340,000 Nm³ per hour.

**Gas POx contributing to clean air**
Our natural gas partial oxidation technology (GasPOx) enables the reduction of carbon, NOx and CO emissions compared to conventional syngas solutions. The technology has been successfully proven in a first reference project in Germany.
Our commitment to safety

We have one goal with respect to health, safety, the environment and security:
to achieve zero accidents and zero environmental incidents.

We ensure that every action we undertake, from initial design to construction, reflects
our goal of ensuring safety and protecting the environment.

In pursuit of this goal, we strive to:

• Provide a safe and secure work environment
• Prevent all injuries, damage to the environment and damage to property
• Identify and reduce risks and exposure to hazards in a sustainable way
• Improve our Health, Safety, Environment and Security performance continuously
• Enforce Air Liquide Life Saving Rules

Embodying a safety-first culture

• Our safety commitment applies not only to our employees, but also to our contractors,
customers, adjacent facilities and local communities.
• We ensure that safety is the responsibility of everyone and is a part of the Air Liquide
Engineering & Construction culture driven by our behavioral-based ACT (Actively
Caring Together) program. In this way, we are all safety leaders, and all share a
commitment to the golden rule of safety first.
• We will not hesitate to stop an activity of whatever nature (design, engineering,
construction execution, or manufacturing) if it is not safe or if there is any suspicion
that it may result in an accident or incident, now or in the future.
Our commitment to sustainability

We strive to contribute to a more sustainable world.

In line with Air Liquide’s Corporate Sustainability Program and in order to contribute to a cleaner industry, transportation and enabling cleaner production, we offer a comprehensive portfolio of environmentally-optimized, efficient and easy-to-use solutions for our customers:

• Cryogenic CO₂ capture technology.
• Methanol production from CO₂ rich feedstock and hydrogen.
• Wide experience in the use of LNG, deployed as clean fuel. Our Liquefin™ technology offers 10% efficiency gain vs. state-of-the-art.
• Our SMR-X for export steam free H₂ production reduces natural gas use and CO₂ emissions by about 5% compared to conventional steam reforming.
• Our vast oleochemicals portfolio is a key-enabler to produce clean chemicals.

Supporting sustainability also involves actions in our own activities in engineering, manufacturing or on our sites to minimize environmental impact, leveraging new ways of digital transformation.
We have the experience, flexibility and capacity to provide a wide range of air separation units through standard plants, customized offerings and other cryogenic liquefaction technologies. Our strength lies in our ability to adapt our plants performances, safety and construction design philosophy to each project/customer specifics.
**Application**
Steel making (basic oxygen furnaces, blast furnaces, electric arc furnaces), chemicals (ethylene oxide, ammonia, etc.)

**Feedstock**
Air + Energy (electrical or steam)

**Product**
Oxygen from 99.6% to 99.8% purity and up to 50 bar

**Co-product**
Nitrogen, liquid oxygen, liquid nitrogen, liquid argon, compressed dry air

**Capacity**
330 to 770 tpd

**Economics**
Specific energy: 400 to 600 kWh/t
Capex: 22 to 30 mm USD

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**Description**
The Yango™ air separation unit is based on air compression, adsorption purification, cryogenic distillation of main components and internal compression of high pressure products.

Yango is a standardized, highly packaged ASU solution to support short-time-to-start-up projects.

Several process schemes are available to optimize both Capex and Opex depending on customer product requirements, energy cost and customer process integration potential.

Air Liquide Engineering & Construction offers optimized solutions in terms of construction strategy, operating philosophy and reliability.

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**Contact**
airgases@airliquide.com
Sigma – Standard Air Separation Unit

**Application**
Steel making (oxygen boosting, electric arc furnace), chemicals (ethylene oxide, etc.), glass, non-ferrous metals, waste water treatment, pulp and paper

**Feedstock**
Air + Energy (electrical)

**Product**
Oxygen up to 99.8% purity

**Co-product**
Nitrogen, liquid oxygen, liquid nitrogen, liquid argon, compressed dry air

**Capacity**
110 to 380 tpd

**Economics**
Specific energy: 280 to 460 kWh/t
Capex: 5 to 9 mm USD

**Description**
Sigma units are based on air separation with the following steps: air compression, adsorption, purification, cryogenic distillation of main components, internal compression. Several process schemes are available to optimize both Capex and Opex depending on customer product requirements. The Sigma units are designed to reduce construction and time to production with a highly packaged architecture. Some liquid co-production could be available to refill backup liquid storages.

**References**
>40

**Contact**
airgases@airliquide.com
Vacuum Swing Adsorption (VSA)  
On-Demand Oxygen Generation

**Application**  
Steel making, glass, pulp and paper, waste water treatment, mining

**Feedstock**  
Air + Energy (electrical)

**Product**  
Oxygen from 90% to 93% purity

**Co-product**  
None

**Capacity**  
40 to 130 tpd

**Economics**  
Specific energy: 265 kWh/t  
Capex: 1 to 6 mm USD

**Description**  
VSA uses the process of air separation by adsorption. The basic principle of air separation by adsorption relies on the use of specific zeolite adsorbents for the selective adsorption of nitrogen over oxygen and argon.

**Main features:**  
- Compact design layout  
- Fully packaged and pre-tested skids  
- Minimized schedule, erection and start-up times  
- Automatic and unattended operation  
 Capitalization of more than 20 years of operating and maintenance experience.

**References**  
>100

**Contact**  
airgases@airliquide.com
Nitrogen Generation System

**Application**
LNG terminal, crude oil refinery, electronics

**Feedstock**
Air + Energy (electrical)

**Product**
Nitrogen (gaseous, liquid) with 100 ppm to 1 ppb O₂

**Co-product**
LOX high purity

**Capacity**
500 Nm³/h to 70,000 Nm³/h of nitrogen

**Economics**
Specific energy: 175 to 280 KWh/t
Capex: 2 to 11 mm USD

**Description**
This nitrogen generation system is based on air separation with the following steps:
- air compression,
- adsorption,
- purification,
- cryogenic distillation of main components.

Several process schemes are available to optimize both Capex and Opex depending on customer product requirements.

Some liquid co-production could be available to refill backup liquid storages.

Systems often include backup vaporizers and storage designed as per customer’s requirements (availability and reliability).

These systems are safe, reliable and easy-to-operate and maintain.

**References**
> 100

**Contact**
airgases@airliquide.com
Large Air Separation Unit

**Application**
Steel making (basic oxygen furnaces, blast furnaces, electric arc furnaces), gas monetization (gas-to-methanol, propylene, liquids), coal gasification, chemicals (ethylene and propylene oxide, etc.), clean power (IGCC, oxycombustion)

**Feedstock**
Air + Energy (electrical or steam)

**Product**
Oxygen up to 99.8% purity and 100 bara

**Co-product**
Nitrogen, rare gases (Kr, Xe, He, Ne), liquid oxygen, nitrogen and argon, compressed dry air

**Capacity**
Up to 6,000 tpd

**Economics**
Specific energy: 160 to 500 kWh/t
Capex: 40 to 300 mm USD
Several processes are available to optimize economics depending on product requirements, energy cost and process integration.

**Description**
Large air separation units are based on adsorption purification, cryogenic distillation of main components and internal compression of high pressure products. From the small standard of a few hundred tonnes per day to Mega ASU complexes (multi-train) of more than 15,000 tonnes per day, Air Liquide Engineering & Construction offers optimized solutions in terms of construction strategy, operating philosophy and reliability.

**References**
>4000

**Contact**
airgases@airliquide.com
Our technologies for rare gases use the most efficient, safe and reliable processes to achieve optimal production or extraction of products. Our solutions are fully integrated into existing plants providing optimal cost and energy efficiencies.
**Krypton / Xenon**

**Description**
Liquid oxygen from ASU(s) is first treated in a primary module, named “Extraction cold box,” which aims to remove contaminants such as N₂O and partially CnHm before entering in a first set of cryogenic separation to produce a pre-concentrated mixture.

The secondary module, named “Krypton-Xenon upgrader,” treats the pre-concentrated mixture through a hydrocarbons purifier before entering into the final concentrated cryogenic separation in order to produce a krypton-xenon mixture enriched at > 98% (rest is oxygen).

This concentrated cryogenic mixture (typically Kr 91%, Xe 7%, O₂ 2%) is then compressed and vaporized to fill gas cylinders at 150 barg.

Final separation (pure Kr, pure Xe) is done outside the ASU plant in a dedicated laboratory.

**Note:** Krypton-Xenon production is economically favored for large ASU (>4000 tpd) or for multi ASUs due to the low Krypton and Xenon content in the air (resp. 1.1 ppm, 0.086 ppm).

**Main features:**
- Integration with ASU
- Low power consumption
- Pre-assembled packages or skid units to ease the erection

**References**
> 10

**Contact**
raregases@airliquide.com
**Helium Extraction and Liquefaction**

**Application**
Pure liquid helium production and loading into ISO containers

**Feedstock**
Natural gas or impure helium gas extracted as non-condensable side-product from LNG units or impure helium gas extracted from nitrogen rejection units

**Product**
Liquid helium

**Co-product**
None

**Capacity**
Up to 20 tpd (one train)

**Economics**
The highly efficient process combined with the vapor recovery system allows for a very high helium recovery (> 99%).

**Capex:** 40 to 300 mm USD

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**Description**
The impure helium feed gas is purified in a first section, where N₂, CH₄, H₂, CO, Ar, O₂, water and CO₂ are separated from helium. It is composed of a cryogenic partial condensation unit, a hydrogen removal system and a Pressure Swing Adsorber (PSA) unit. Then, the pure gaseous helium is cooled and liquefied via a helium cycle and the use of cryogenic expanders with a highly optimized cryogenic exchanger arrangement. Expanders are based on a proprietary technology using static gas bearing, ensuring high reliability and efficiency. Liquid helium is continuously produced and stored in tanks. The unit is equipped with loading bays to fill ISO containers. All helium vapors from the containers are collected and recycled within the unit.

**Contact**
raregases@airliquide.com
Cryocap™ is a technological innovation for CO₂ capture using a cryogenic process involving low temperatures, around -50°C, combined with membranes separation, that is unique in the world. It can be adapted to specific applications combining a variety of Air Liquide technologies: the capture of CO₂ produced by thermal power plants (Cryocap™ Oxy), or hydrogen production units (Cryocap™ H₂).
Overview

Cryocap™ Oxy

Hydrogen & Syngas Generation

Oxycombustion

Cryocap™ H₂ #24

H₂ or Syngas

CO₂ for CCS

Carbon-free Flue Gas

Cryocap™ Oxy #25

CO₂ for CCS
Cryocap™ H₂ – Cryogenic CO₂ Separation

Application
CO₂ capture from H₂ production plants

Feedstock
Offgas from H₂ plant

Product
CO₂

Co-product
H₂

Capacity
From 500 to 2,000 tpd

Economics
Opex + Capex:
- 45 USD/tonne of CO₂
- Increase H₂ production by 13% to 20%
- Cryocap™ H₂ offers the lowest costs for CO₂ production from H₂ plant (20% less capex than amines)

Description
The offgas is compressed, dried and sent to a cryogenic unit, where the CO₂ is separated from the other components by a combination of partial condensation and distillation. A pure and pressurized CO₂ flow is produced from the cold box.

The non condensed gases are recycled through a membrane system to recover H₂ and CO₂. Residual gas is sent to the burners of the reformer.

The CO₂ product is compressed up to supercritical pressure or liquefied and stored in liquid storage.

Food-grade quality can be achieved by an additional purification on a catalytic bed where all remaining hydrocarbons and alcohols are destroyed.

Cryocap™ H₂ can be installed for greenfield as well as brownfield H₂ plants.

Main feature:
- More than 98% of CO₂ recovery from syngas

Reference
1 (100 000 t/y)

Contact
cryocap@airliquide.com

Natural gas
SMR
H₂ - PSA

Fuel
Cold Box

Residue to fuel gas

Cryocap™ H₂

Food-grade quality can be achieved by an additional purification on a catalytic bed where all remaining hydrocarbons and alcohols are destroyed.

Cryocap™ H₂ can be installed for greenfield as well as brownfield H₂ plants.

Main feature:
- More than 98% of CO₂ recovery from syngas

Reference
1 (100 000 t/y)

Contact
cryocap@airliquide.com
Cryocap™ Oxy – Cryogenic CO₂ Separation for Oxycombustion

Description
The flue gas issued from the boiler plant is first treated in a pre-treatment unit, which aims to cool the gas and remove the SOx, HF, HCl, most of the NOx, and the dust. Then the gas is compressed and dried before entering the cryogenic purification unit.

In the cold box, CO₂ is recovered by combination of partial condensation and distillations, which allow the removal of the heavy compounds such as NOx and the light elements such as O₂, Ar, N₂, NO and CO.

The CO₂ product is compressed, condensed and pumped up to supercritical pressure.

Main feature:
• More than 98% of CO₂ recovery from syngas

References
3 (from 25 000 to 1.2 million t/y)

Contact
cryocap@airliquide.com

Application
CO₂ capture from power plants

Feedstock
Oxycombustion flue gas

Product
CO₂

Co-product
None

Capacity
From 1,000 to 15,000 tpd

Economics
Cryocap™ Oxy allows very high CO₂ recovery and near zero-emission to the atmosphere (SOx, particulate matters, NOx, Hg).

Capex: 40 to 300 mm USD
We are pushing technology limits in design and delivery of syngas plants, including the world's largest units. Our plants meet the needs of large, medium, and small customers with a wide range of possible steam export rates.
Overview

Lurgi FBDB™
Coal
Hydrogen & Syngas Separation

Lurgi MPG™
Natural gas
LPG
Naphtha

Liquid residue
from oil refining

Gas POX
Autothermal Reformer
Steam Methane Reformer

Rectisol

CO₂ Capture

Chemicals

Hydrogen & Syngas Separation

#28 #29 #30
#31
#32
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#34
#35
Steam Methane Reforming (SMR)

**Application**
Generation of syngas by steam reformation of methane rich hydrocarbon

**Feedstock**
LPG, naphtha, natural gas, refinery off-gas

**Product**
Hydrogen, carbon monoxide, syngas or a combination thereof

**Co-product**
Steam, optionally carbon dioxide

**Capacity**
Per SMR train:
- 15,000 - to 200,000 Nm³/h H₂ plant
- 3,500 - 40,000 Nm³/h CO plant
- Up to 350,000 Nm³/h syngas

**Economics**
Opex:
- H₂ plants (based on nat. gas feed & fuel): Steam co-export ratio: 0.4 to 1.1 kg/Nm³ H₂
- Feed+Fuel: 14.5 to 15.3 MJ/Nm³ H₂
- HyCO plants (based on nat. gas feed & fuel): H₂/CO product ratio: 2.6 to 4.2
- Steam co-export ratio: 0.3 to 0.7 kg/Nm³ \([H₂+CO]\)
- Feed+Fuel: 14.2 to 14.8 MJ/Nm³ \([H₂+CO]\)

Capex:
- H₂ and HyCO plants (incl. purification): 25 to 370 mm USD

**Description**
Feedstocks are desulfurized, mixed with steam and pre-heated.
Optionally a catalytic pre-reforming step may be foreseen to convert the feed/steam mixture to a methane rich gas to improve efficiency of the SMR.
The main reforming reaction takes place in the proprietary top-fired steam reformer in which the feed/steam mixture is converted while passing catalyst filled and heated tubes at temperatures of 800 to 940 °C and pressures of 15 to 45 barg.
Reformed gas leaving the reformer contains H₂, CO, CO₂ and unreacted components.
Efficiency of the process and composition of the reformed gas can be adjusted via the process parameters reforming pressure, temperature and steam to feed ratio.
In case H₂ yield should be increased or maximized a catalytic shift reactor may be added and fed with reformed gas to convert CO and steam to additional H₂ and CO₂.
In case a high CO yield is targeted CO₂ may be separated from reformed gas and recycled to the SMR. Additional import CO₂ may be added if available.
Suitable product purification technologies include: PSA and membrane for H₂, amine wash (aMDEA) for CO₂ removal and methane wash Cold Box for CO.

**Main features:**
- Flexibility in process design to optimize for best efficiency, lowest Capex or lowest total cost of ownership
- Optimized integration of refinery off-gases for H₂ production and recovery
- Best in class plant reliability and operability through operational feedback from Air Liquide’s own plants.

**References**
> 140 (> 40 in last 20 years)

**Contact**
hydrogen-syngas@airliquide.com
Small-Scale Standard Hydrogen Plant

**Description**

The small-scale standard H₂ plant product is based on hydrogen production via steam reforming of hydrocarbon feedstocks. Additionally, a CO-shift and PSA unit are included to maximize the H₂ yield and purify the H₂. For more details regarding the process technology reference is made to the description of Steam Methane Reforming (SMR).

The small-scale standard H₂ plant product includes four different plant sizes with pre-defined equipment, piping arrangement and lay-out.

Its design is optimized for minimum total cost of ownership, but nevertheless allows for considerable process flexibility.

The product is suitable for receiving different types of feedstocks, its configuration may be selected for high or low steam co-product ratios with an option for high export steam quality. A pre-reformer may be included as well, particularly in combination with liquid feedstocks.

**Main features:**

- Design of standard plant allows for considerable process flexibility
- High degree of modularization to limit exposure during construction
- Compact plant layout and small foot-print
- Delivery time < 15 month FOB from project award

**References**

>20 (6 in last 10 years)

**Contact**

hydrogen-syngas@airliquide.com

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**Application**

Hydrogen production by steam reforming in a highly standardized and modularized plant

**Feedstock**

Natural gas, refinery off-gas, LPG, naphtha

**Product**

Hydrogen

**Co-product**

Steam

**Capacity**

15,000 - to 45,000 Nm³/h H₂

**Economics**

Opex: Feed+Fuel: 14.5 to 15.0 MJ/Nm³ H₂ (Figures based on nat. gas feed & fuel)

Capex: 25 to 60 mm USD
SMR-X™ – Zero Steam Hydrogen Production

**Description**

SMR-X technology is based on a new generation steam methane reformer furnace with additional heat recovery of the reformed gas leaving the reaction zone back to the catalyst bed. To achieve this, the reformed gas passes via heat exchange tubes, located inside the main reformer tubes, before leaving the reformer. Geometry and material of the internal heat exchange system is optimized for high efficiency and reliability. Consequently, utilization of SMR-X allows for a H₂ plant design with balanced steam production and consumption at superior overall process efficiency compared to conventional SMR technology. Also, highly efficient H₂ plant designs with very low steam co-export ratios are possible. Furthermore, the plant’s steam system is simplified and the reformer size of SMR-X is reduced compared to a conventional furnace, because approximately 20% of the required process heat is supplied by internal heat exchange.

**Main features:**
- H₂ plant de-coupled from steam host
- Highest efficiency of all available zero steam solutions
- >5% reduction of CO₂ emissions compared to conventional SMR based zero steam design
- Attractive plant Capex due to compact reformer design

**Contact**

hydrogen-syngas@airliquide.com

**Application**

Production of hydrogen in a radiative heat exchange steam methane reformer (SMR) without co-export of steam

**Feedstock**

Natural gas, refinery off-gas, LPG, naphtha

**Product**

Hydrogen

**Co-product**

None (optionally steam at low co-export ratio)

**Capacity**

Up to 100,000 Nm³/h hydrogen

**Economics**

Opex:
Feed+Fuel: Appr. 13.6 MJ/Nm³ H₂
(Figures based on nat. gas feed & fuel)

Capex:
25 to 135 mm USD
**ATR – Autothermal Reforming**

**Description**
Desulfurized feed gas is preheated and optionally pre-reformed prior to entering the ATR reactor. The gas is fed via the proprietary burner into a refractory-lined reactor operating at 30 to 100 barg, where it reacts with oxygen and steam to form syngas. The syngas is further reformed via a Ni-based catalyst bed located in the same reactor. The syngas is cooled in a waste heat boiler producing high pressure steam. Depending on the needed syngas properties of the downstream process this technology can be applied as stand-alone ATR or as a combination of SMR and ATR known as Combined Reforming.

**Main Features:**
- Provide large quantities of H₂-rich gas at lowest cost
- Compact reactor
- High pressure (up to 100 bar)

**References**
>30

**Contact**
hydrogen-syngas@airliquide.com
Gas POX – Natural Gas Partial Oxidation

Description
Feed gas is desulfurized, mixed with steam and preheated in a fired heater. Feed, steam and oxygen are fed from the proprietary burner to a refractory lined reactor operating at up to 100 barg, where H₂, CO and CO₂ are produced via partial oxidation. Reformed gas is cooled down producing high pressure steam. CO₂ is removed from the syngas in an amine wash unit. In case a high CO yield is targeted CO₂ may be separated from syngas and recycled to the POx. Additional import CO₂ may be added if available. Suitable product purification technologies include: PSA and membrane for H₂, oxogas, amine wash (aMDEA) for CO₂ removal and partial condensation Cold Box for CO.

Main Features:
• Efficient technology for products with low H₂/CO ratio or for pure CO production
• Revamp of residue POx reactors allows for switching to more economic nat. gas feed
• Low CO₂ footprint

References
6

Contact
hydrogen-syngas@airliquide.com
Lurgi MPG™ – Multi-Purpose Gasifier

Description
The feedstock together with oxygen and steam is fed via the proprietary MPG-burner into the refractory lined entrained flow reactor operating at 30 to 100 barg, where it reacts in a non-catalytic partial oxidation at typically 1,200 to 1,500 °C to form syngas. The syngas leaving the bottom of the reactor is cooled by quench or in a waste heat boiler, depending on feedstock characteristics and downstream usage.

The proprietary MPG-burner design allows a wide variety of feedstock properties to be handled safely and reliably, covering high viscosity and even occasional particles up to millimeter size. The pressurized water cooling of the burner insures safe operation under all conditions. The technology may also be adapted to the usage of slurries with solid content or bio-based syncrude.

Main Features:
- Valorization of residues capable of converting almost any liquid feedstock
- Highly tolerant to impurities
- High pressure

Contact
hydrogen-syngas@airliquide.com
Lurgi FBDB™ – Fixed Bed Dry Bottom Coal Gasification

**Application**
Gasification of coal to produce syngas

**Feedstock**
Lumpy coal, especially suited for low-rank (high ash, high water) coal

**Product**
Syngas (H₂+CO), due to high CH₄ content, particularly suited for the production of SNG (synthetic natural gas) or DRI (direct reduction of iron ore)

**Co-product**
Crude tar acids (phenols), sulfur, tar, oil, naphtha, ammonia

**Capacity**
40,000 to 120,000 Nm³/h dry syngas per gasifier, typically more than 5 reactors per plant, largest plant 40 reactors at one site.

**Economics**
Individual costs depend strongly on location, coal quality, etc.

**Yield:**
2000 Nm³ dry syngas / ton dry coal

**Capex:**
420 to 650 mm USD (cost base: 7 Mk+ in China)

**Description**
Coal is converted into syngas by reacting in a counterflow fixed bed with oxygen and steam. The raw syngas will be further processed (CO-shift, Rectisol™) to meet the downstream requirements of the processes. Side streams are further treated using proprietary technologies to produce valuable co-products, as well as to meet environmental specifications. Special water treatment allows for zero liquid discharge while minimizing water consumption.

**Main Features:**
- Robust technology that can be fed with coarse lumps, avoiding the need for grinding and drying
- Higher cold gas efficiency than entrained flow gasification
- Wide variety of coal possible
- Lower water consumption than entrained flow gasification

**References**
>100 gasifiers

**Contact**
hydrogen-syngas@airliquide.com
Rectisol™ – Syngas Purification

Description

Acid gases in raw gases from any gasification are removed by absorption with a physical solvent (cold methanol). The rich solvent leaving the contactor is regenerated by flashing and stripping. Different process configurations are available to deliver a tailored solution optimized for Capex and Opex for a given syngas specification.

Rectisol™ is the leading process when it comes to the purification of gasification-based syngas for catalytic applications (production of SNG, methanol, ammonia, or Fischer-Tropsch) as well as hydrogen.

Using inexpensive solvent in combination with optimized heat integration, the Rectisol process has extremely low operating costs and high availability.

Main Features:

- Highest level of purity for all contaminants
- Low Capex and Opex when compared to other purification process
- Low cost solvent
- CO₂ offgas meeting most stringent emissions requirements

References

> 110 (> 35 since 2005)

Contact

hydrogen-syngas@airliquide.com
Leveraging on our vast technology portfolio, we have the means to combine various patented processes to address any Hydrogen & Syngas separation challenge. Our customers benefit from continuous improvements due to Air Liquide’s own track record in its operational experience of such processes - from cryogenics to permeation to adsorption.
Overview

Hydrogen & Syngas Generation

- H₂ Offgas (Refineries, Crackers, PHD...)

- Pressure Swing Adsorption PSA #38
- H₂ Membrane #42
- Liquid Nitrogen Wash #41
- Hydrogen Liquefier #43
- CO Cold Box Methane Wash #39
- CO Cold Box Partial Condensation #40

- Pure H₂
- Ammonia Syngas (N₂/H₂)
- Liquid Hydrogen
- Pure CO
- Oxogas
- Hydrogen
Pressure Swing Adsorption (PSA) 
Hydrogen Purification

Application
Recovery and purification of pure hydrogen from different H₂-rich streams

Feedstock
Raw hydrogen from SMR, POX, cryogenic purification, methanol plant purge gases, ethylene off-gas, styrene offgas, gasification, ammonia plant, CCR, and other offgases or any combination of the above

Product
Hydrogen up to 99.9999% purity

Co-product
None

Capacity
5,000 to 200,000 Nm³/h

Economics
H₂ recovery rate: 60 to 90%
Opex: Feed+Fuel: Appr. 13.6 MJ/Nm³ H₂ (Figures based on nat. gas feed & fuel)
Capex: 1 to 5 mm USD

Description
Pure H₂ product is delivered at a pressure close to feed pressure (pressure drop across PSA could be as low as 0.5 bar) and impurities are removed at a lower pressure (typical PSA offgas pressures range from 1.1 to 10 bara).
The PSA tail-gas, containing impurities, can be sent back to the fuel system (SMR burners or refinery fuel network) with or without the need of a tail-gas compressor. Operation is fully automatic.
PSA units use the most advanced adsorbents on the market and patented high efficiency cycles to provide maximum recovery and productivity. Typical on-stream factors are >99.9%.
Turndown can be as low as 25%.
PSA units are compact, fully skid-mounted and pre-tested units designed for outdoor and unmanned operation.

References
>70 (in operation or under construction)

Contact
hydrogen-syngas@airliquide.com
CO Cold Box – Methane Wash

**Application**
Carbon monoxide (CO) production or ratio-adjusted synthesis gas production from synthesis gas for use in chemical industry

**Feedstock**
Synthesis gas from natural gas, naphtha or coal/residue.

**Product**
CO up to 99.99% purity

**Co-product**
Hydrogen, oxogas, methane, LNG

**Capacity**
Up to 34,000 Nm³/h (1020 tpd) CO

**Economics**
**Opex:** Specific energy: 300 to 600 kWh/tonne
**Capex:** Economics are highly dependent on the type and quality of feedstock (coal, naphtha or natural gas), as well as the required CO purity and pressure (MDI/TDI, PC, AcAc, MEG, etc.) and of the required scope of supply.

**Description**
Methane Wash process is based on cryogenic separation technology using the difference in boiling points of the main components from the synthesis gas.
Feed gas is pretreated to remove impurities which will freeze at cryogenic temperatures encountered in the process. It is then cooled down in heat exchangers and washed with liquid methane before being purified step by step through distillation columns.
Every cryogenic process is tailor-made to fit the customer’s specifications and other requirements on co-products.

**Main Features:**
- Greatest number of references in CO/N₂ separation
- Highest safety standards for all Cold Boxes
- In-house technology for highly safe, highly reliable & highly efficient CO expander
- High CO recovery

**References**
32 (latest 2016)

**Contact**
hydrogen-syngas@airliquide.com
CO Cold Box – Partial Condensation

Application
Carbon monoxide (CO) production or ratio-adjusted synthesis gas production from synthesis gas for use in chemical industry.

Feedstock
Synthesis gas from natural gas/naphtha or coal/residue gasification.

Product
CO up to 99.99% purity

Co-product
Hydrogen, oxogas, methane, LNG

Capacity
Up to 55,000 Nm³/h (1,650 tpd) CO

Economics
Opex:
Specific energy: 18 to 100 kWh/tonne

Capex:
Economics are highly dependent on the type and quality of feedstock (coal, Naphtha or natural gas), as well as of the required CO purity and pressure (MDI/TDI, PC, AcAc, MEG, etc.) and of the required scope of supply.

Description
Partial Condensation process is based on cryogenic separation technology using the difference in boiling points of the main components from the synthesis gas. Feed gas is pretreated to remove impurities which will freeze at cryogenic temperatures encountered in the process. It is then partly condensed in heat exchangers and flashed in a syngas drum before being purified step by step through distillation columns. Every cryogenic process is tailor-made to fit the customer’s specifications and other requirements on co-products.

Main Features:
- Greatest number of references in CO/N₂ separation
- Highest safety standards for all cold boxes
- Low specific energy consumption for wide range of feedstock

References
17 (latest 2017)

Contact
hydrogen-syngas@airliquide.com
Liquid Nitrogen Wash

**Description**

Raw hydrogen and high pressure nitrogen are fed to the liquid nitrogen wash unit. Both streams are cooled down against product gas.

Raw hydrogen is fed to the bottom of the nitrogen wash column and condensed nitrogen liquid is fed to the top. Trace impurities, like methane, argon and carbon monoxide, are removed and recycled as fuel gas.

To establish the desired H₂/N₂ ratio, high pressure nitrogen is added to the process stream.

**Main Features:**
- Highest safety standards for all Cold Boxes
- Low specific energy consumption for Methane / LNG co-production

**References**

49 (latest 2015)

**Contact**

hydrogen-syngas@airliquide.com
Hydrogen Separation Membranes

**Application**
Recovery of hydrogen in refinery or chemical plants purge gas
H₂ / CO ratio adjustment

**Feedstock**
Any purge gas streams with hydrogen concentrations >20 % (vol).

**Product**
Hydrogen (>99% vol achievable)

**Co-product**
None

**Capacity**
Membrane systems are truly scalable with virtually no upper capacity limit Largest system referenced by Air Liquide: 124 membrane cartridges

**Economics**
Opex:
- Dependant on feedstock quality
- Hydrogen recovery > 98%
- 50% + turndown capabilities

Capex:
1 mm to 10 + mm USD

**Description**
Our membranes operate on the basis of selective permeation. Each membrane is composed of millions of polymeric hollow fibers similar in size to the diameter of a human hair. The “fast gases,” or gases with a higher permeation rate, permeate through the membrane into the hollow interior and are channeled into the permeate stream. Simultaneously, the “slower gases” flow around the fibers and into the residue stream. As a result, the fibers have the ability to selectively separate a fast gas like hydrogen from carbon monoxide, methane, heavier hydrocarbons and other slower gases.

The process begins when pressurized feed gas is routed to the coalescing filter to remove contaminants and protect the membranes’ fiber from liquid aerosols and particulates. Feed gas is then preheated before entering the membranes. The membranes then separate the feed into the hydrogen-rich permeate and hydrogen-lean residue. The separation of permeate and residual gas is driven by the hydrogen partial pressure difference between the feed gas and permeate gas, as well as our advanced polymer material. The non-porous hollow fiber membranes selectively allow faster molecules to permeate the membrane wall while slower, bulkier molecules remain on the high pressure side.

**Main Features:**
- No moving parts
- Skid mounted systems cartridge design for simple installation
- Estimated payback period of less than a year
- High permeability membranes for compact, low capital system design
- Unrestrained turndown capabilities
- Linear scale up for all size systems
- Hollow fiber membranes offer higher area to volume efficiency resulting in better packing efficiency, smaller footprint and reduced weight and module count.

**Contact**
hydrogen-syngas@airliquide.com
Hydrogen Liquefier

**Description**

Hydrogen to be treated may come from different sources. Accordingly, source warm purification upstream cold purification and liquefier by itself may be required.

Hydrogen is precooled thanks to N₂/MR cycle and the use of turbo-expander together with cryogenic exchangers.

The liquefier uses BAHX (widely used in cryogenic gas liquefaction).

Then it is cooled and liquefied thanks to a H₂ cycle and the use of cryogenic expanders together with a highly optimized cryogenic exchangers’ arrangement. The particularity of hydrogen liquefaction is the use of catalyst to convert ortho-hydrogen into para-hydrogen in order to reduce boil-off in storage.

Boil-off from LH₂ storage is sent back into H₂ cycle, in order to recover molecules.

Downstream infrastructure (storages, loading bays, etc.) can also be supplied.

**Contact**

hydrogen-syngas@airliquide.com

**Application**

Liquefaction of all kinds of H₂ stream for the filling of H₂ liquid storages which ease transportation of H₂ molecules

**Feedstock**

Many sources: natural gas, coal, or electrolyse

**Product**

Liquid hydrogen

**Co-product**

None

**Capacity**

Up to 50 TPD

**Economics**

Opex: Less than 10kWh/kg LH₂
Using our expertise and patents in catalytic conversion and purification techniques, we provide technology to produce or to separate valuable intermediate chemicals from syngas and other feedstock. Our experience and continuous development of our products ensures well referenced safe and reliable technology for our customers that can be tailored to meet their specific needs.
Overview

- **Any carbonaceous feedstock**

**Syngas Generation**

- **Lurgi Methanol** #46
  - Methanol
- **Lurgi MegaMethanol™** #47
  - Propylene
- **Lurgi MTP™** #48
  - Acrylic Acid
  - Methyl Acrylate
  - Ethyl Acrylate
  - Butyl Acrylate
  - 2-EH Acrylate
- **Acrylic Acid** #50
  - Acrylates #51 #52 #53 #54
- **Gas to Gasoline (G2G™)** #49
  - Gasoline
- **Raffinate-2 C4 stream from FCC or MTO/MTP**
  - Butene to Crude Butadiene #55
  - Butadiene Extraction #56
  - Butadiene
- **Crude C4**
- **Pyrolysis Gasoline**
- **Urea**
- **Distapex™** #57
  - Benzene, Toluene, Xylene
- **Melamine** #58
  - Melamine
**Lurgi™ Methanol**

**Application**
Medium-scale production (< 1 million tpa) of methanol from synthesis gas derived from all kinds of carbonaceous material

**Feedstock**
Natural gas or synthesis gas (H₂+CO)

**Product**
Methanol in the required specification (AA, IMPCA, etc.)

**Co-product**
None

**Capacity**
Up to 3,500 tpd

**Economics**
Natural gas consumption: 29 MMBTU (LHV)/tonne (this includes energy for the process, all utilities and the ASU that produces 0.4 - 0.5 tonne O₂/tonne methanol)

Capex: 250 to 500 mm USD

**Description**
In the LP methanol unit (either with integrated gas generation based on natural gas or downstream of a coal gasification unit) syngas is converted over a copper catalyst in water-cooled reactor to produce raw methanol. Unconverted synthesis gas is recycled back to the synthesis loop to enhance yield and carbon efficiency. Raw methanol leaving the synthesis loop is further distilled to meet the required specification.

**Main Features:**
- Simple to operate over full catalyst life time
- Optimized heat transfer preventing temperature peaks in the methanol reactor
- Flexible integration with any syngas generation

**References**
>40

**Contact**
chemicals@airliquide.com

Note: scheme represents only the methanol synthesis unit
Lurgi MegaMethanol™

**Application**
Large scale production (> 1 million tpa) of methanol from synthesis gas derived from all kinds of carbonaceous material

**Feedstock**
Natural gas or synthesis gas (H₂+CO)

**Product**
Methanol in the required specification (AA, IMPCA, etc.)

**Co-product**
None

**Capacity**
2,500 to 7,000 tpd
10,000 tpd (GigaMethanol)

**Economics**
Natural gas consumption: 29 MMBTU (LHV)/tonne (this includes energy for the process, all utilities and the ASU that produces 0.4 - 0.5 tonne O₂/tonne methanol)

**Capex:**
400 to 1100 mm USD

**Description**
In the Lurgi MegaMethanol™ unit (either with integrated gas generation based on natural gas or down-stream of a coal gasification unit) syngas is converted over a copper catalyst in a two-stage reactor system (water-cooled followed by gas-cooled) to produce raw methanol. Unconverted synthesis gas is recycled back to the synthesis loop to enhance yield and carbon efficiency.

Raw methanol leaving the synthesis loop is further distilled to meet the required specification.

Due to high energy integration of the unit and the low recycle ratio in the synthesis loop, Lurgi MegaMethanol™ yields the lowest production cost.

Our most recent design (GigaMethanol) can produce up to 10,000 tpd in one single train.

**Main Features:**
- Methanol loop with minimized recycle ratio resulting in reduced piping and equipment
- Process intensification through interstage condensation possible
- Best referenced technology in the 5000 mtpd class

**References**
9 in operation (5 gas based, 4 coal based),
4 in construction (2 gas based, 2 coal based).

**Contact**
chemicals@airliquide.com

Note: scheme represents only the methanol synthesis unit
**Description**

In a first step, methanol is converted into dimethyl-ether (DME) which is, together with recycled hydrocarbon streams, the feedstock for the fixed-bed MTP reactor filled with proprietary zeolite catalyst. The effluent from the MTP reactor is cooled and enters a separation sequence similar to the one applied in steam-crackers. During this sequence, the effluent is separated into different hydrocarbon streams which are partially recycled to the reactor in order to maximise the propylene yield. The last step of the separation sequence yields polymer-grade propylene.

Compared to crude-based processes (naphtha cracking, metathesis, PDH) the MTP process has the lowest cash cost.

**Main Features:**
- Focus on propylene product
- Lowest cash cost
- High integration potential with methanol and other technologies

**References**

3 in operation (all coal based), first natural gas based plant in engineering stage.

**Contact**

chemicals@airliquide.com
G2G™ – Gas-to-Gasoline

**Application**
Lurgi MegaMethanol™ and ExxonMobil MTG technologies are licensed in an integrated approach to monetize low cost feedstock, usually natural gas or coal, to high value oil products. Air Liquide can also leverage its global network of ASUs and syngas facilities to provide synergistic solutions for G2G™ projects.

**Feedstock**
Natural gas (NG), coal, heavy hydrocarbons, biomass

**Product**
Sulfur free gasoline/petrol

**Co-product**
LPG (optional)

**Capacity**
1,000 to 32,000 bpd
Standardized design: 16,100 bpd

**Economics**
Yield: 9,100 scf natural gas/barrel
Opex: 8.5 USD/barrel
Capex: 250 to 2000 mm USD

**Description**
G2G™ technology presents an opportunity to monetize low cost feedstock into transportation fuels either for domestic use or for export markets. Projects are driven by the spread between the price of feedstock and oil products. Low cost gas or stranded gas can enhance profitability even at low-moderate oil price scenarios. The gasoline product from G2G™ is low in benzene and has no sulfur compounds. Product can be used as on-spec gasoline that meets or exceeds any typical (stringent) environmental standards or as a refinery blending stock.

Profitability is driven by low feedstock prices relative to market value of wholesale oil products.

**Contact**
g2g@airliquide.com
**Application**
The combined Lurgi/Nippon Kayaku technology produces ester-grade acrylic acid (EAA). Main uses are adhesives, paints and coatings (acrylic esters).

**Feedstock**
Propylene

**Product**
Ester-grade acrylic acid

**Co-product**
None

**Capacity**
Up to 20 t/h (single train)

**Economics**
Capex: 200 to 300 mm USD

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**Description**

**Reaction:** Acrylic acid (AA) is produced by catalyzed oxidation of propylene in a two-stage tubular fixed-bed reactor system. The reactors are cooled by circulating molten heat transfer salt. The heat of reaction is used to produce steam.

**Quench:** The AA is recovered from the reactor product gas in a quench tower. The AA solution is routed to an extractor. Uncondensed gases are sent to an offgas treater to recover the remaining AA. A side draw from the offgas is sent to incineration. Overhead gas is recycled to the first reactor.

**Solvent extraction:** Liquid-liquid extraction is used to separate water and AA. The solvent is recovered and recycled. In a first step, water and acetic acid are removed to achieve a crude AA to be further purified in the next process steps. The extractor bottom is sent to the raffinate stripper to recover remaining solvents.

**Crude AA recovery:** In this section, solvent and acetic acid are removed from crude AA using two columns.

**Raffinate stripping:** The raffinate stripper recovers solvents from the wastewater streams. The Lurgi/Nippon Kayaku technology combines high performance catalysts with highest acrylic acid yields and outstanding catalyst longevity with an optimized process. With low raw material and energy consumption, low environmental impact and high onstream time, this technology exhibits competitive production costs.

**Acrylic acid purification:** Crude AA is purified in the ester grade AA column. To maximize AA recovery, dimer is converted to AA in a dedimerizer.

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**References**

1

**Contact**

chemicals@airliquide.com
Methyl Acrylate (Synthomer Licensed)

**Application**
Production of methyl acrylate (MA) by the esterification reaction of acrylic acid with methanol (MeOH). The methyl acrylate is used mainly for adhesives, paints and coatings.

**Feedstock**
Acrylic acid, methanol

**Product**
Methyl acrylate

**Co-product**
None

**Capacity**
Up to 4 t/h

**Economics**
Process configuration is optimized resulting in low raw material consumption, optimized energy integration and low utility requirements. Environmental impact minimized. On stream times exceeding 8,000 hours per year could be achieved.

**Description**

The reaction is catalyzed in a fixed bed reactor by means of a strong acid solid catalyst (ion-exchange resin).

The reactor effluents are routed to the fractionation section to separate unreacted acrylic acid from crude methyl acrylate, process water and methanol. Further purification of the crude methyl acrylate takes place in the alcohol extractor and the light ends column where process water and methanol, as well as other light ends, are removed. The final product column separates high boiling components to be routed to the AA recovery section and the purified MA product can be send to storage.

In the AA regeneration section acrylic acid is recovered to be recycled to the reactor.

The high boiling components are routed to the decomposer where they could partly be converted back to methanol, methyl acrylate and acrylic acid to be recycled. Remaining unconverted components are discharged to battery limit for further treatment.

The bottom product of the alcohol extractor is routed to the methanol regeneration section to recover methanol to be recycled to the reactor. The water is partly reused in the process as well as routed to battery limit for further treatment.

Methyl acrylate is prone to polymerization. In order to minimize polymerization effects, an inhibitor injection system is foreseen at critical locations in the plant.

**References**

1

**Contact**

chemicals@airliquide.com

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**Diagram Notes**

- AA: Acrylic Acid
- MA: Methyl Acrylate
- MeOH: Methanol
- Catalyst
- Alcohol Extractor
- Alcohol Recovery Column
- Light Ends Column
- Final Product Column
- Decomposer
- Organic Residue
- Waste Water
- AA Recovery Column
Ethyl Acrylate (Synthomer Licensed)

**Application**
Production of ethyl acrylate (EA) by the esterification reaction of acrylic acid with ethanol (EtOH). The ethyl acrylate is used mainly for adhesives, paints and coatings.

**Feedstock**
Acrylic acid, ethanol

**Product**
Ethyl acrylate

**Co-product**
None

**Capacity**
Up to 4 t/h

**Economics**
Process configuration is optimized resulting in low raw material consumption, optimized energy integration and low utility requirements. Environmental impact minimized. On stream times exceeding 8,000 hours per year could be achieved.

**Description**
The reaction is catalyzed in a fixed bed reactor by means of a strong acid solid catalyst (ion-exchange resin).
The reactor effluents are routed to the fractionation section to separate unreacted acrylic acid (AA) from crude ethyl acrylate, process water and ethanol. Further purification of the crude ethyl acrylate takes place in the alcohol extractor and in the light ends column where process water and ethanol as well as other light ends are removed. The final product column separates high boiling components to be routed to the AA recovery section and the purified EA product can be sent to storage.
In the AA regeneration section the acrylic acid is recovered and recycled to the reactor. The high boiling components are routed to the decomposer where they are partly converted back to ethanol, ethyl acrylate and acrylic acid to be recycled. Remaining unconverted components are discharged to battery limit for further treatment.
The bottom product of the alcohol extractor is routed to the EtOH regeneration section to recover ethanol to be recycled to the reactor. The water is partly reused in the process as well as routed to battery limit for further treatment. Ethyl acrylate is prone to polymerization. In order to minimize polymerization effects, an inhibitor injection system is foreseen at critical locations in the plant.

**References**
1

**Contact**
chemicals@airliquide.com
Butyl Acrylate (Synthomer Licensed)

**Description**

The reaction is catalyzed by means of para-toluene sulphuric acid (PTSA). A four stage reactor system ensures the conversion. The process water generated by the reaction is continuously removed from the reactor system. Process water, unconverted butanol and acrylic acid leaving the reactor system are separated in the dehydration columns. The organic phase (mainly butanol and AA) is recycled. The liquid crude BA and the catalyst are routed to the catalyst extraction column where the catalyst is extracted by means of process water and is recycled to the reactors. Residual acrylic acid in the crude BA is neutralized in the neutralization column by means of a caustic soda solution.

In the purification section light ends are removed from the crude BA and recycled back to the reactor system. In a second step high boiling components are separated and the final pure BA product is generated to be sent to storage. The high boiling components are transferred to the decomposer where they could partly be converted back to mainly BA to be recycled to the reactor section. Remaining unconverted components are discharged to battery limit for further treatment.

Butyl acrylate is prone to polymerization. In order to minimize polymerization effects, an inhibitor injection system is foreseen at critical locations in the plant.

**References**

1

**Contact**

chemicals@airliquide.com
2-Ethylhexyl Acrylate (Synthomer Licensed)

**Application**
Production of 2-ethylhexyl acrylate (2EHA) by the esterification reaction of acrylic acid with 2-ethylhexanol (2EHOH). The 2EHA produced is used mainly for adhesives, paints and coatings.

**Feedstock**
- Acrylic acid, 2-ethylhexanol

**Product**
- 2-ethylhexyl acrylate

**Co-product**
- None

**Capacity**
- Up to 5 t/h

**Economics**
Process configuration is optimized resulting in low raw material consumption, optimized energy integration and low utility requirements. Environmental impact minimized. On stream times exceeding 8,000 hours per year could be achieved.

**Description**
The reaction is catalyzed by means of para-toluene sulphuric acid (PTSA). A three stage reactor system ensures the conversion. The process water generated by the reaction is removed continuously by an azeotropic distillation step with a carrier agent. The reactor effluent which contains the reacted 2EHA, non-reacted 2EHOH and PTSA is routed to the extraction section where the PTSA catalyst is extracted by means of process water and recycled to the Catalyst Regeneration Column. Additional 2EHOH is introduced via this column into the process and the extraction water is separated. The recovered PTSA catalyst and the preheated 2EHOH is routed to the first reactor. In the coalescer section water is removed from the extracted crude 2EHA. The following purification section separates unreacted alcohol which is recycled to the reaction section. Furthermore, high boiling components are removed and the final pure 2EHA product is generated to be sent to storage. The high boilers are discharged to the heavy end decomposer where they are partly converted back to 2EHA and 2EHOH and recycled to the reactor section. Remaining unconverted components are discharged to battery limit for further treatment. 2EHA is prone to polymerization.

In order to minimize polymerization effects, an inhibitor injection system is foreseen at critical locations in the plant.

**References**
1

**Contact**
chemicals@airliquide.com
Butene-to-crude Butadiene (Mitsubishi BTcB Process)

Application
The BTcB process produces crude butadiene by oxidative dehydrogenation of butenes.

Feedstock
Raffinate 2 from naphtha cracker
Butene rich C4 from FCC units
C4 by-product of MTO/MTP units

Product
1,3-butadiene

Contact
chemicals@airliquide.com

References
1 pilot plant

Description
The butene rich feedstock is oxidatively dehydrogenated in a fixed bed reactor using air and steam. After quenching the reactor effluent, remaining oxygen, oxygenates and other impurities are removed.

The produced crude butadiene is routed to a BASF NMP butadiene extraction unit for further purification to generate the final high purity 1,3-butadiene product.

The Mitsubishi BTcB process combines high conversion rates and high selectivity while operating at mild reaction conditions.
**Butadiene Extraction (BASF NMP Licensed)**

**Application**
Recovery of 1,3 butadiene from a crude C4 stream from olefins plants by extractive distillation.

**Feedstock**
Crude C4

**Product**
1,3 butadiene

**Co-product**
None

**Capacity**
6 to 35 t/h

**Economics**
Utility consumption:
- Steam: 1.7 t/t
- Electricity: 150 kWh/t
- Water, cooling: 150 m³/t

**Capex:** 80 to 110 mm USD

**Description**
In the pre-distillation tower methyl acetylene, propadiene and other light components are separated from the C4 cut feedstock which then enters the bottom section of the main washer column while NMP solvent enters at the top. C4 raffinate consisting of butanes and butenes is drawn off as overhead product. The loaded solvent is sent to the rectifier. In the first compartment of the divided wall column, the less soluble butenes are separated and recycled to the main washer while C4 acetylenes are separated from crude butadiene in the second compartment. The solvent from the rectifier is sent to the degassing tower where hydrocarbons are stripped from the solvent and then recycled to the rectifier by a compressor. The side stream of the degassing tower containing diluted C4 acetylenes is fed into a scrubber to recover NMP solvent. After further dilution with raffinate or other suitable materials, the C4 acetylene stream is discharged to battery limits for further processing. The crude butadiene withdrawn as overhead product from the second compartment of the rectifier is sent to the butadiene column for final purification. The butadiene product is withdrawn as liquid side product.

**Ecology:** NMP biodegrades readily and has low toxicity to aquatic life. Compared to other technologies, this process is much more eco-friendly. In addition the BASF SELOP selective hydrogenation process can be offered for further treatment of the C4 Acetylene stream to increase the 1,3 Butadiene yield.

**References**
>36

**Contact**
chemicals@airliquide.com
Distapex™ – Aromatics Extractive Distillation

**Description**

The aromatics in the feedstock are separated by extractive distillation using N-methylpyrrolidone (NMP) as a solvent. The raffinate product containing the non-aromatics leaves the extractive distillation column via the top. The loaded solvent is routed to a stripper column where the final aromatic product is recovered at the column top and routed to battery limit. The lean solvent is recycled to the extractive distillation column.

**Ecology:**

Due to the unique properties of NMP, the process has an excellent ecological footprint and requires medium pressure steam only. The Distapex™ process requires a minimum number of equipment items and is especially renowned for reliability and availability as well as low operating costs.

**References**

>27

**Contact**

chemicals @airliquide.com
**Lurgi/Edgein Melamine**

**Application**
The Lurgi/Edgein low pressure technology produces melamine from urea in a catalytic vapor-phase reaction. Main uses are laminates, adhesives and coating.

**Feedstock**
Urea

**Product**
Melamine

**Co-product**
None

**Capacity**
Up to 7.5 t/h in a single train

**Economics**

**Consumption per metric ton of melamine:**
- Urea melt: 3.15 tons, net value 1.5 tons
- Ammonia: 0.3 tons
- Catalyst: 4 kg
- HP steam: 0.5 tons
- Electrical power: 1300 kWh
- Natural gas: 15.5 GJ (ca. 397 Nm³)
- Cooling water: 33 tons
- No quench water required
  (no waste water)

**Capex:** 185 mm USD

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**Description**

Molten urea is fed to a fluidized bed reactor using a silica/aluminum oxide catalyst. The fluidization is accomplished with an ammonia/CO₂ mixture to process off-gas. The required heat for the reaction is provided by circulating molten salt through internal heating coils. The gaseous reactor effluent is cooled to a level that the by-products and the catalyst fines can be removed in a filtration step. The solid melamine particles are generated by desublimation in a crystallizer and are finally separated by a cyclone. The off-gas is recycled to a urea washing tower where it is scrubbed with molten urea before being partially recycled as fluidizing gas to the reactor and as quench gas to the crystallizer section. Surplus on off-gas can be recycled to the upstream urea plant or a separate off-gas treatment unit.

The melamine produced with the Lurgi/Edgein technology is characterized by an excellent quality, with small particle sizes and a uniform particle size distribution exceeding the standard requirements for the downstream applications.

**References**

>13

**Contact**

chemicals@airliquide.com
Raw natural gas needs to be treated to meet pipeline and liquefaction specifications. We offer a full range of technologies to remove any kind of contaminant, offering clients a reliable and cost-effective solution tailored to their needs.
Overview

CO₂ Removal
- Cryocap Membranes
- Membranes

Acid Gas (Sulfur, Mercaptans) Removal
- Amine Wash
- Omnisulf
- Purisol

NGL Recovery
- Turbobooster Membranes

Sulfur

LNG
- Natural Gas
- Liquid Helium
- Helium
- Nitrogen
- NGL
**Acid Gas Removal – Amine Wash**

**Application**
Removal of acid gases (CO₂, H₂S, COS, light mercaptans) from natural gas, associated gases and unconventional gas sources.

**Feedstock**
Natural gas

**Product**
Sweet natural gas

**Co-product**
Acid gases

**Capacity**
Up to 1,500,000 Nm³/h

**Economics**
Economics are highly dependent on feedstock and requirements (high efficiency or low Capex).

Contact us for more information

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**Description**
Acid gases contained in raw gases are removed by absorption with a chemical or a mixture of chemical and physical solvent. The rich solvent leaving the contactor is regenerated by flashing and stripping.

The process configuration and solvent selection will be tailored according to feedstock and sweet gas application.

Air Liquide Engineering & Construction can offer very energy-efficient processes such as the BASF OASE® purple or formulated MDEA for pipeline or liquefied natural gas specifications.

This process presents the advantage of very low hydrocarbon co-absorption.

**References**
> 50

**Contact**
gas-treatment@airliquide.com
Acid Gas Removal – OmniSulf™

Description
The OmniSulf™ technology encompasses the following proprietary key processes:

- Acidic components are removed using BASF’s OASE® technology and the cleaned gas is routed to a dehydration and mercaptan removal unit (DMR) that removes moisture and mercaptans with multi-layered bed of specialized zeolitemolecular sieves. If necessary, mercury is removed from the sweet gas with impregnated activated carbon. Mercaptans are recovered from the regeneration gas with the Lurgi Purisol™ technology.
- The liquid sulfur product is degassed to H₂S concentrations below 10 ppm by applying the Aquisulf™ technology.

Offgases are incinerated before being released to the atmosphere.

The OmniSulf™ technology can be tailored for gas reinjection.

Contact
gas-treatment@airliquide.com

Application
Sweetening and processing of natural gas by removing CO₂, H₂S, COS, mercaptans, water and mercury to pipeline or LNG specifications as well as production of liquid elemental sulfur while minimizing SO₂ emissions to the atmosphere to meet most stringent environmental regulations.

Feedstock
Raw natural gas, associated gas

Product
Dry sweet gas, sulphur (99.9+% purity)

Co-product
None

Capacity
Up to 1,500,000 Nm³/h

Economics
Economics are highly dependent on feedstock and requirements (high efficiency or low Capex).

Contact
gas-treatment@airliquide.com
Acid Gas Removal – Purisol™

**Description**

The Purisol™ process uses a highly selective, non-toxic, non-corrosive, easily available solvent (N-Methyl-2-Pyrrolidone, NMP) for the physical absorption of the undesired acidic components of a feed gas or process gas, like H₂S and mercaptans. The process requires very low Opex due to several features. Taking advantage of the very high selectivity towards H₂S and mercaptans compared to CO₂ and hydrocarbons allows a low circulation rate. The process is operated at ambient temperature and thus does not need high cooling duty. Regeneration of the solvent is done by flashing and heating. Because of the high boiling point of the solvent, losses are extremely low.

A typical application is the cleaning of periodically released regeneration gases of natural gas treatment to a clean fuel gas. Here an additional feature is to provide a continuous flow of sulfur rich gas to the Claus process by using the buffering function of the setup.

The process can be modularized and also easily be integrated into existing plants.

**Main Features**:

- Non-toxic, non-corrosive solvent, easily available solvent
- Smooth and peakless gas to Claus process

**Contact**

gas-treatment@airliquide.com

**Application**

Highly selective removal of acid gases (H₂S, mercaptans, etc.) from natural gas and process gases

**Feedstock**

Natural gas, regeneration gas, process gas

**Product**

Clean sulfur free gas

**Co-product**

Sulfur rich gas for SRU

**Capacity**

50 000 - 500 000 Nm³/h

**Economics**

Individual costs vary significantly depending on capacity and purity request

Opex: This process has typically very low Opex due to the high selectivity and easy regeneration as well as a stable solvent with low losses due to high boiling point

Capex: 3 to 40 mm USD
CO₂ Removal – Cryocap™ NG

**Description**

The CO₂ rich natural gas is first dried and sent to a cold box where it is cooled down and sent to a distillation column. High CO₂ partial pressure favors the CO₂ partial condensation and thus makes its separation from natural gas even easier. The non-condensable gas is enriched in methane and sent to a membrane for final purification. The CO₂ purity of the product corresponds to pipeline specifications, generally 1 to 10 mol%. The permeate stream of the membrane enriched in CO₂ is sent back to the cold box. The CO₂ and heavy hydrocarbons condense in the cold box and are collected at high pressure. NGL recovery is possible with almost no additional cost.

Cryocap™ NG is tolerant to a few % H₂S. Cryocap™ NG also allows for H₂S bulk removal from NG.

**Contact**

gas-treatment@airliquide.com

**Application**

Removal of CO₂ from natural, associated gases and unconventional gas sources

**Feedstock**

Natural gas with high CO₂ content (> 35%)

**Product**

Natural gas

**Co-product**

CO₂ (under pressure)
NGL (possible)

**Capacity**

Up to 1,000,000 Nm³/h

**Economics**

Separation cost: less than 1 USD/MMBTU
Capex savings:
> 50% vs. amine absorption (at high CO₂ content)
Contact us for more information.
CO₂ Removal – Membranes

**Application**
CO₂ removal from natural gas

**Feedstock**
Natural gas with moderate to high acid gas content

**Product**
Sweet natural gas

**Co-product**
Acid gases

**Capacity**
Up to 500,000 Nm³/h

**Economics**
Economics are highly dependent on feedstock and requirements (high efficiency or low Capex). Contact us for more information.

**Description**
Air Liquide Engineering & Construction offers a vast portfolio of gas separation membranes for natural gas treatment: the natural gas product is recovered as a high-pressure retentate while the impurities are concentrated in the low pressure permeate. This includes bulk CO₂ removal with the highly selective MEDAL™ NG, as well as H₂ dewpointing, bulk CO₂ removal and dehydration with PEEK-SEP™ suite of products.

**Main Features:**
The hollow-fiber type offers more compact and robust membrane solutions to meet pipeline specifications. Air Liquide membrane technology is characterized by higher resistance to hydrocarbons and higher selectivity, compared to cellulose acetate products, offering higher methane recovery, lower investment and operating costs.

**Contact**
gas-treatment@airliquide.com
**Description**

Air Liquide Engineering & Construction offers open-art or proprietary natural gas liquids technologies (NGL) for high efficiency C₂ recovery (>98%), high propane recovery (99+%), and low energy consumption. Air Liquide know-how and operational expertise of key technology components (heat exchangers, turbo-expander) allow for robust and reliable solutions. Additionally, Air Liquide can combine NGL recovery with its nitrogen rejection technology and expertise in cryogenics to provide overall optimized NGL/NRU plants.

**Contact**

gas-treatment@airliquide.com

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**Application**

NGL (C₂+) recovery from natural gas, associated gases and unconventional gas sources

**Feedstock**

Lean or Rich Natural gas

**Product**

Ethane, LPG, condensates, natural gas

**Co-product**

LNG, crude helium

**Capacity**

Up to 1,000,000 Nm³/h

**Economics**

Increased NGL recovery with significant reduction in capital and/or operating costs as compared to open-art technologies. Contact us for more information.
Natural Gas Liquids Recovery – Membranes

**Application**
NGL recovery from rich gas and fuel gas conditioning (including dewpointing and BTU value adjustment)

**Feedstock**
Natural gas, associated gases, unconventional gas sources, refinery off-gas, flared gas

**Product**
Treated natural gas, NGL

**Co-product**
Fuel gas

**Capacity**
Up to 100,000 Nm³/h

**Economics**
Air Liquide membrane solutions are characterized by low investment and operating costs that can translate into short payback periods.

Contact us for more information.

**Description**
Thanks to outstanding mechanical properties of the PEEK-SEP™ membranes, liquid C3+ can be recovered at high pressure whereas the residual gas is produced as a low pressure permeate. The membrane system is simple and reliable, and does not require extensive feed gas pre-treatment beyond an inlet coalescing filter.

PEEK-SEP™ membranes can also be used as a pretreatment stage upstream of MEDAL™ NG (CO₂ removal units) to optimize the performance and reduce overall footprint and weight as compared to traditional pre-treatment schemes. Other applications of the PEEK-SEP™ membranes include hydrocarbon dewpointing (the treated gas is produced at high-pressure) and nitrogen removal for BTU value adjustment purposes.

Air Liquide’s membrane solutions represent a robust and compact option to unlock the use of low quality fuel gas and the monetization of valuable Natural Gas Liquids (NGL) contained in rich gas sources such as flared gas, refinery off-gases or fuel gas networks.

When the feed gas is rich in heavy hydrocarbons, typical refrigeration plants can be attractive when sufficient NGL liquid product can be recovered.

Air Liquide POROGEN PEEK-SEP™ membranes provide alternative solutions to recover NGLs even when the amount of NGLs is too low to allow for economic recovery by traditional means.

Contact

gas-treatment@airliquide.com

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**Application**
NGL recovery from rich gas and fuel gas conditioning (including dewpointing and BTU value adjustment)

**Feedstock**
Natural gas, associated gases, unconventional gas sources, refinery off-gas, flared gas

**Product**
Treated natural gas, NGL

**Co-product**
Fuel gas

**Capacity**
Up to 100,000 Nm³/h

**Economics**
Air Liquide membrane solutions are characterized by low investment and operating costs that can translate into short payback periods.

Contact us for more information.

**Description**
Thanks to outstanding mechanical properties of the PEEK-SEP™ membranes, liquid C3+ can be recovered at high pressure whereas the residual gas is produced as a low pressure permeate. The membrane system is simple and reliable, and does not require extensive feed gas pre-treatment beyond an inlet coalescing filter.

PEEK-SEP™ membranes can also be used as a pretreatment stage upstream of MEDAL™ NG (CO₂ removal units) to optimize the performance and reduce overall footprint and weight as compared to traditional pre-treatment schemes. Other applications of the PEEK-SEP™ membranes include hydrocarbon dewpointing (the treated gas is produced at high-pressure) and nitrogen removal for BTU value adjustment purposes.

Air Liquide’s membrane solutions represent a robust and compact option to unlock the use of low quality fuel gas and the monetization of valuable Natural Gas Liquids (NGL) contained in rich gas sources such as flared gas, refinery off-gases or fuel gas networks.

When the feed gas is rich in heavy hydrocarbons, typical refrigeration plants can be attractive when sufficient NGL liquid product can be recovered.

Air Liquide POROGEN PEEK-SEP™ membranes provide alternative solutions to recover NGLs even when the amount of NGLs is too low to allow for economic recovery by traditional means.

Contact

gas-treatment@airliquide.com
Nitrogen Rejection Unit

**Application**
Removal of nitrogen from natural gas, associated gases and unconventional gas sources

**Feedstock**
Natural gas with high nitrogen content

**Product**
Natural gas, nitrogen

**Co-product**
LNG, liquid nitrogen, crude helium

**Capacity**
Up to 1,000,000 Nm³/h

**Economics**
Economics are highly dependent on feedstock and requirements (high efficiency or low Capex).

Contact us for more information.

**Description**
Natural gas feed is partially condensed, then methane and nitrogen are separated into a system of distillation column(s). Depending on the feed composition and pressure, the system can include one to three distillation columns. The process scheme selection is done according to project-specific parameters such as feed evolution with time and product specifications. Air Liquide Engineering & Construction offers a wide range of solutions, such as the ability to treat any N₂/CH₄ mixtures (5-90%), high efficiency, flexibility and recovery (>99% methane), minimization of greenhouse gas emissions to the atmosphere (methylene in N₂ vent << 1%). Capex optimization and operation flexibility are allowed thanks to proprietary design and Air Liquide operational feedback.

**References**
>15

**Contact**
gas-treatment@airliquide.com
Hydrogen sulphide removed in the Natural Gas Cleaning or Crude Oil Refining can be converted into pure sulfur product using proven Claus technology. Over the years, we have developed a highly efficient and reliable burner system and further technologies to boost this traditional process, making it more efficient, less costly and more environmentally friendly.
Oxynator™ / OxyClaus™ for Sulfur Recovery Units (SRU)

Description
In a conventional Sulfur Recovery Unit ambient air is used to oxidize part of the hydrogen sulfide (H₂S) in the acid gases to sulfur dioxide (SO₂). By enriching the combustion air to the Claus unit with pure oxygen more feed gas can be processed in the SRU without violation of pressure drop or residence time constraints. Air Liquide Engineering & Construction provides the most suited oxygen enrichment technology depending on client’s requirements.

Oxynator™ for low-level enrichment (<28% O₂ in air)
Low-level oxygen enrichment is a very cost effective option to increase SRU capacity up to 125% as there is usually no modification required on existing SRU equipment. Air Liquide uses its patented Oxynator™, a compact swirl type mixer, for safe and efficient oxygen mixing. The oxygen is injected into the combustion air upstream of the Claus burner.

OxyClaus™ for high-level enrichment (<60% O₂ in air)
Capacity increase to 200% can be achieved by using the well known Lurgi OxyClaus™ process that can safely handle high levels of oxygen. In the specially designed Lurgi OxyClaus™ burner the oxygen is directly injected into the flame via dedicated oxygen lances. The hot oxygen flame is surrounded by a cooler acid gas – air flame shielding the refractory from exposure to high temperature.

Main Features:
• Integration with ASU
• Low power consumption
• Pre-assembled packages or skid units to ease the erection

References
>40

Contact
sulfur@airliquide.com
**Description**

The acid gases are burnt sub-stoichiometrically with air in a refractory lined furnace. Resulting mixture of H₂S and SO₂ reacts to form elemental sulfur which is removed from the process through condensation. In subsequent catalytic stages, typically two or three, the conversion to sulfur is promoted further yielding a sulfur recovery of 94.5% – 97.5% for the Claus unit. Two tail gas treatment (TGT) options are available to boost the sulfur recovery further.

1) **Sulfreen™**: A sub-dewpoint, catalytic purification of the Claus tail gas for an overall sulfur recovery of up to 99.5%.

2) **LTGT™**: Claus tail gas is purified in a wet-scrubbing process. Due to the recycling of the H₂S rich stream to the Claus unit, total sulfur recovery can be increased to 99.9%.

In the degassing section, the H₂S content of the liquid sulfur is decreased to less than 10 ppm. For this the catalytically promoted Aquisulf™ technology can be employed.

Offgas from tail gas treatment and degassing is incinerated and released to the atmosphere.

**References**

>170 Claus plants (4 to 1,000 tpd)
>60 tail gas treatment processes
>50 Aquisulf™ in operation

**Contact**

sulfur@airlique.de
Emission-Free Sulfur Recovery Unit

Application
Recovery of sulfur from acid gas streams containing hydrogen sulfide (H₂S) with 100% sulfur recovery

Feedstock
Acid gases from acid gas removal unit and sour-water strippers

Product
Bright yellow sulfur with up to 99.9% purity

Co-product
None

Capacity
Up to 1,000 tpd

Economics
Capex: 25% less than conventional amine-wash tail gas treatment
Sulfur recovery: 100%

Contact us for more information.

Description
Raw gas is desulfurized in an AGR and the removed acid gas is sent to the emission-free SRU for sulfur recovery. The oxygen based Claus process is employed to recover sulfur from the acid gas in elemental form. The recovered sulfur is degassed and is then available as a sellable product.

Claus tail gas is hydrogenated and cooled before being compressed and routed back to the AGR. Here it is desulfurized and the H₂S is recycled together with the acid gas back to the Claus unit. Other valuable components inside the tail gas, like H₂ and CO end up in the purified gas. With this recycle a sulfur recovery rate of 100% is achieved. The sulfur emissions to the atmosphere in the overall complex are significantly reduced.

OxyClaus™ is used in this concept because this reduces the process gas volume and therefore lowers not only investment cost plus operating cost but also the amount of inert gas sent to AGR.

References
3 emission-free SRUs have been designed, two are in operation.

Contact
sulfur@airliquide.com
As an expert in cryogenics and a pioneer in the field of Liquefied Natural Gas, we have extensive experience in equipping plants of all sizes with LNG technology. Our modularized designs are easy to construct and our robust liquefaction technology based on cold boxes helps reduce costs.
Overview

Natural Gas Treatment

Liquefaction

Small

Nitrogen Cycle Turbofin™ #76

Single Mixed Refrigerant Smarfin™ #77

Dual Mixed Refrigerant Liquefin™ #78

Large

BOG Reliquefaction #79

Downstream

Bunkering Stations #80

Air Liquide Engineering & Construction

Technology Handbook
**Turbofin™ (Nitrogen Refrigerant Cycle)**

**Application**
Liquefaction of natural gas for small scale plants serving power applications (peak shaving, remote power) or fuel (marine, truck, rail, etc.)

**Feedstock**
Natural gas

**Product**
LNG

**Co-product**
NGLs, depending on feedstock composition

**Capacity**
Up to 0.25 Mtpa

**Economics**
Opex: Typically 450 kWh/ton of LNG

**Description**
The process consists of three main modules: pre-treatment of natural gas (NG), liquefaction and LNG storage and loading (truck, trailer, bunkering barge, etc.).

1) The pre-treatment consists mainly of CO₂ and H₂O removal. It is either a simple Temperature Swing Adsorption (TSA) cycle or a combination of amine wash with TSA depending on the CO₂ content in the feed gas.

2) The liquefaction process is based on a nitrogen cycle (closed loop): N₂ is first compressed and boosted. After being cooled down through a Brazed Aluminum Heat Exchanger, it is expanded releasing N₂ at low pressure and low temperature. Cold N₂ (T<-165°C) is then re-injected into the main Heat Exchanger to cool down the NG and convert it to LNG which is sent to storage. Warm N₂ is then recycled through the cycle compressor.

3) Storage can either be fabricated for small volumes (vacuum insulated) or site erected flat bottom tanks for larger needs, depending on the applications considered. The loading station can be adapted to truck, trailer, or maritime. Regasification is added downstream of the storage for peak shaving facilities.

**Main Features:**
- Cost effective especially for small scale plant
- Non-hydrocarbon refrigerant improving safety
- Simplicity of operation

**References**
90

**Contact**
lng@airliquide.com

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**Diagram:**
- Feed Gas
- Gas Treatment
- Scrubber
- HC Condensates
- Brazed Aluminium Heat Exchanger
- LNG Storage
**Description**

Smartfin™ is a single mixed refrigerant type of process optimized with the use of Brazed Aluminium Heat Exchangers (BAHX).

The refrigeration cycle is filled with a mixture of hydrocarbons and nitrogen.

The refrigerant is compressed and separated in liquid and gaseous streams. Lightest fractions of the refrigerant are sent to the cold end of the main heat exchanger, cooled down and sent back to the compressors after being vaporized through the main BAHX. Heaviest fractions are let down and vaporized at an intermediate level in the main BAHX.

The optimization of the mixed refrigerant cycle consists of taking advantage of the vaporization temperature difference between generated refrigerant streams to optimize the natural gas liquefaction heat exchange profile. In addition, the heavy hydrocarbons removed from the process can be recovered and sold as NGL.

**Main Features:**

- Efficient Process
- Reduced number of rotating machines
- Flexibility of Operation

**References**

17

**Contact**

lng@airliquide.com
**Description**

Liquefin™ is a Dual Mixed Refrigerant type of process optimized with the use of Brazed Aluminium Heat Exchangers (BAHX).

Each of the two refrigeration cycles is using a dedicated mixture of refrigerant.

The first cycle is filled with a fluid composed of relatively heavy components (HMR, an ethane and propane mixture). The second cycle uses a fluid made of lighter components (LMR, a nitrogen, methane and propane mixture). Each HMR and LMR fluid is compressed through a compressor, cooled and introduced in the Cold Box under a single phase. The HMR is then let down in several stages, generating the cooling duty that pre-cools the Natural Gas (NG) and condenses the LMR at about -70°C. No phase separation of LMR is necessary which means a simpler scheme and a better operability. The LMR is then also let down, generating the cold duty that allows for NG liquefaction and sub-cooling at about -160°C.

The proprietary Main Cryogenic Heat Exchanger is a Cold Box mainly composed of compact multi-fluid BAHX and vessels.

**Main Features:**
- The most efficient liquefaction process
- Low capital cost
- Modular design, lowering construction risk.

**Contact**

lng@airliquide.com
Boil-Off Gas Reliquefaction Units

**Description**
A boil-off gas (BOG) reliquefaction unit allows recovery of BOG emitted from LNG storage by relquefying it.

Several systems are proposed, either using liquid nitrogen or nitrogen expansion cycle as cooling agent.

Typical relquefaction capacity is in the range 2-40 tons per hour.

Such units avoid BOG flaring, and debottlenecking of LNG export terminals. They can also reduce the cost of terminal by avoiding investment in BOG compressors.

**Contact**
lng@airliquide.com

**Application**
Reliquefaction of Boil-Off Gas (BOG) on import & bunker terminals

**Feedstock**
Boil-Off Gas

**Product**
Reliquefied Boil-Off Gas

**Capacity**
2 to 40 T/h

**Economics**
Typical power consumption 400 to 800 kWh/ton
Bunkering Stations

**Application**
- LNG as bunker fuel
- LNG for truck distribution
- LNG for remote power generation

**Feedstock**
- Liquid natural gas

**Product**
- Liquid natural gas / natural gas

**Co-product**
- None

**Capacity**
- 500 to 10,000 m³ storage capacity

**Economics**
- Opex: N/A

**Description**

A distribution hub is used to import small quantities of LNG and distribute them to various downstream users such as ships, trucks, or power plant.

A set of several vacuum insulated tanks with a maximal capacity of 1000 m³ each are used, minimizing site work and allowing phasing of the capacity.

A proprietary boil-off gas management (BOG) system ensures that no gas is lost during operation of the hub and that the fuel remains as dense and low pressure as possible during the storage.

Equipments ensuring the interface with ship (loading arm) and trucks (proprietary Turbo-Bay) are included in the scope of supply. LNG pumps, transfer lines, metering device and regasification system (if needed) are also provided.

Downstream infrastructure (LNG trucks, refueling station, regas satellite station) can also be supplied.

**Main Features:**
- Proprietary BOG management technology without need for BOG compressors
- Proprietary transfer systems

**Contact**

lng@airliquide.com
Our leading edge technologies provide complete system processing, from seed crushing and oil extraction to oil refining for a wide range of downstream applications. Air Liquide Engineering & Construction oleochemical technologies create value for the food, cosmetics, detergents, surfactants and pharmaceutical industries through our comprehensive offering.
Overview

Oil / Fats
- Refining #85
  - Glycerin Distillation & Bleaching #89
    - Methyl Ester Distillation / Fractionation #87
      - Biodiesel
      - Methyl Esters
      - Pharma Glycerin
    - Bio Propylene Glycol #92
      - Bio Propylene Glycol
    - Methyl Ester Hydrolysis #88
      - Fatty Acids
      - Fatty Alcohol
    - Fatty Alcohol LP3 #91
      - Edible Oil
    - Fatty Acid #90

Oil seeds
- Seed Crushing and Extraction #84
  - Sorbitol #93
  - Glucose

Sorbitol
- Glucose

Edible Oil
- Sorbitol
Seed Crushing and Extraction
Lurgi Sliding Cell Extractor

**Application**
Production of crude edible oils

**Feedstock**
Oil seeds (soybean, canola/rapeseed, sunflower, palm kernel...)

**Product**
Crude edible oils for use in food or technical applications after refining
Meal for animal feed

**Co-product**
Crude lecithin

**Capacity**
Up to 5,000 tpd

**Economics**
Economics are highly dependent on the type of feedstock and required meal quality.

**Capex:** 25 to 100 mm USD

**Description**
The oil content of different types of seeds ranges between 20-50% wt. After feedstock specific preparation steps (cleaning, drying, etc.) the oil is gained from the seeds by solvent extraction with hexane. For seeds with higher oil content (e.g., rapeseed, sunflower) the extraction is typically combined with a pre-pressing step to reduce the load on the extraction.

The Lurgi sliding cell extractor is the core of the extraction plant. It provides high flexibility regarding feedstock changes, very reliable operation and optimum extraction conditions with complete counter-current flow of solvent vs. cake and large contact areas.

The miscella (oil/solvent mixture) from extraction is separated into its components by distillation and water degumming. The solvent is reused in the extraction after removing the collected moisture. Gums can be purified to lecithin or recycled to the meal.

The desolventized, toasted, dried and cooled (DTDC) meal is used as protein rich animal feed.

The whole process is kept under slight vacuum so that emissions are controlled by absorption to fulfill environmental regulations.

**References**
>300

**Contact**
oleo@airlique.com
Natural Oil Refining

Description
Crude oils and fats contain different contaminants like free fatty acids (FFA), phospholipids (gums), soaps, color, odor, etc. Their removal is called “refining” for food purposes to reach RBD oil quality (refined, bleached, deodorized) and “pretreatment” to reach quality for further processing, e.g. for biodiesel production or oil splitting.

Technologies are available for all applications: FFA can be removed chemically by neutralization or thermally by deacidification. Waxes are separated in winterization. Color and polycyclic aromatic hydrocarbons (PAHs) are removed in bleaching; odors and pesticides during deodorization (with vitamin E as potential by-product).

Refining also includes process steps for fat modification like hydrogenation (saturation of double bonds), interesterification (to adjust the melting point) or fractionation (separation according to chain length) and side processes like soapstock splitting or gum drying.

References
>400

Contact
oleo@airliquide.com
**Description**

Biodiesel is produced from triglycerides by transesterification with methanol under presence of an alkali catalyst (sodium methylate) at 60 degrees and atmospheric pressure.

Key features of Lurgi’s biodiesel technology are maximum yield (1 kg feedstock = 1 kg biodiesel), closed wash water loop (no waste water from core process units) and sediment removal for palm and soya oil to remove sterol glucosides far below limits given by international quality standards.

Only NaOH and HCl are used in the process. Resulting sodium chloride ends up in the glycerin, can easily be removed and does not cause fouling or side reactions during further processing (see glycerin distillation).

**References**

>50 (since 2000)

**Contact**

oleo@airliquide.com
Fatty Acid Methyl Ester Distillation/Fractionation

**Description**

Fatty Acid Methyl Ester (FAME) is separated according to molecular chain lengths to apply specific cuts in a fractionation column. A falling film evaporator and vacuum pressure reduce heat stress to FAME resulting in superior product quality suitable for surfactant or personal care applications.

Distilled FAME can also be sold as top-quality water-clear biodiesel with improved cold flow properties and 50-100 ppm residual water. Sterol glucosides and monoglycerides are removed close to detection limits.

Heat recovery by steam generation makes this process very energy efficient.

**References**

>10 (since 2000)

**Contact**

oleo@airliquide.com
Methyl Ester Hydrolysis

**Application**
Conversion of methyl esters to fatty acids

**Feedstock**
Methyl ester fractions

**Product**
Fatty acid fractions

**Co-product**
Methanol

**Capacity**
60 tpd

**Economics**
Low value short-chain methyl esters can be converted to high value fatty acids

**Description**
Methyl ester is mixed with water and hydrolyzed to fatty acid and methanol at 250 °C and 70 bar. Heat recovery reduces the amount of energy used in the process.

The reaction mixture is cooled and separated into an organic phase and a water phase. Both streams are distilled and unreacted methyl ester and water are recycled.

The produced fatty acid is methanol-free and can be sold without further treatment. Methanol is recovered and can be used in the methyl ester production.

**Contact**
oleo@arliquid.com
Glycerin Distillation and Bleaching

Application
Purification of glycerin to pharma and technical grade

Feedstock
Crude glycerin from biodiesel or oil splitting (fatty acid) plants

Product
Pharma grade glycerin (purity > 99.7%)

Co-product
Technical grade glycerin (purity 85-90%)

Capacity
10 tpd to 600 tpd

Economics
Opex: 35 USD/tonne

Description
Vacuum distillation is used to separate glycerin from organic components and salts at temperatures up to 175°C. The residue from the column bottom is sent to a thin film evaporator to increase glycerin yield. Salt can be separated from the residue by a decanter to reduce the amount of waste and to increase glycerin recovery even further. Pharma grade glycerin as main product is polished by bleaching, i.e. adsorption at fixed beds of activated carbon. Light impurities end up in the by-product, technical grade glycerin.

References
> 45

Contact
oleo@airliquide.com
**Fatty Acid**

**Description**

Triglycerides are hydrolyzed catalyst-free to fatty acids and glycerin by addition of water at elevated temperatures (250°C) and elevated pressure (55 bar) with splitting degrees up to 99.5%. The fatty acids from the splitting column are dried by flashing before further processing by distillation/fractionation or hydrogenation. Water and glycerin are also flashed for heat recovery. Final concentration of crude glycerin is 80-88% (almost salt-free), which can be sold or further processed to pharma grade glycerin.

Fatty acids are separated from non-volatile components by vacuum distillation. Fractions of different fatty acid chain lengths with high purity can be obtained with our fractionation plants. The use of structured packing and vacuum in the fractionation columns reduces the thermal stress and ensures high product qualities. Each fatty acid fractionation plant will be tailor-made by our experts to ensure best fit to the needs of our customers.

Hydrogenation of fatty acids is the saturation of fatty acid double bonds by addition of H₂ (~99.9% by vol.) under elevated temperatures and pressure (up to 200°C @ 25 bar) in the presence of a Ni catalyst. This treatment adjusts melting points and enhances storage stability. Continuous (for full hydrogenation and large plants) and batch process variants (for full or partial hydrogenation) are available.

**Application**

Production of fatty acids

**Feedstock**

Seed oils, tropical oils, animal fats

**Product**

Fatty acid

**Co-product**

Glycerin water (25-35% glycerin content)

**Capacity**

100 tpd to 1,000 tpd

**Economics**

Opex: 10 USD/tonne (feedstock) (depending on number of fractions and their related purities)

**References**

>25 (since 2000)

**Contact**

oleo@airliquide.com
Fatty Alcohol “LP3”

**Description**

Fatty alcohols can be produced from fatty acids or methyl ester.

Latest improvement is the use of the hydrogenation step with LP3 features:

- **Liquid Phase**: Proven liquid phase hydrogenation in fixed bed reactors also suitable for long chain fatty alcohols in contrast to vapor phase hydrogenation.

- **Low Pressure**: Comparatively low pressure (reduced from 250 bar to 75 bar) reduces energy requirements (Opex savings approx. 5%) and Capex (savings approx. 15-20%).

- **Long Performance**: Double reactor system for seamless catalyst changeovers with no disruption to operations and efficient catalyst utilization for more profitable lifecycles (see operation steps in diagram).

The temperature in the catalyst beds is controlled by hydrogen quenches to limit amount of side-products.

Traces of oxygenates are hydrogenated in a polishing section (carbonyl conversion). The resulting fatty alcohol cuts can further be fractionated into final fatty alcohol products.

---

**Application**

Improved hydrogenation process for fatty alcohol

**Feedstock**

Fatty acid or methyl ester

**Product**

Fatty alcohol

**Co-product**

None

**Capacity**

90 tpd to 600 tpd

**Economics**

Opex: 100 USD/tonne
Contact us for more information.

---

**Contact**

oleo@airliquide.com

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**References**

8

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**Unsaturated Fatty Alcohol**

As an option, long chain unsaturated fatty alcohols can be obtained retaining 95% of C=C double bonds, based on Methyl Ester route.
Bio Propylene Glycol (BASF Licensed)

Description
In this process, licensed from BASF, glycerin is hydrogenated in liquid phase using a copper catalyst. The reaction takes place in two serial fixed bed reactors at a temperature between 175 to 195 °C and pressures between 75 and 200 bar. The crude product is purified in a two-column distillation unit to yield pharma grade propylene glycol.

References
1 pilot plant
1 commercial demonstration plant
2 plants in engineering phase

Contact
oleo@arliquide.com

Application
Production of bio propylene glycol (1,2-propanediol, MPG) from glycerin as alternative to petrochemical route

Feedstock
Pharma grade glycerin

Product
Pharma grade propylene glycol

Co-product
Technical grade propylene glycol

Capacity
50 to 100 tpd

Economics
Contact us for more information
**Application**
Sorbitol is produced by batchwise hydrogenation of aqueous glucose solution. This technology is also suitable for different sugar alcohols, e.g. Mannitol, Xylitol.

**Feedstock**
Glucose from wet milling plants

**Product**
Technical, food or pharma grade sorbitol

**Co-product**
None

**Capacity**
100 to 200 tpd

**Economics**
Opex: 130-165 USD/tonne w/o feedstock and fixed cost.
Capex: 4 to 7 mm USD

**Description**
The glucose solution is hydrogenated in a batch reactor using nickel or ruthenium catalysts. Reaction takes place at 110°C and 40 bar pressure. After reaction, the product slurry is filtered to recover the catalyst. Makeup catalyst compensates catalyst loss and deactivation. The crude sorbitol solution is purified by ion exchange and evaporated to the final concentration. Optionally, sorbitol powder can be obtained by melt crystallization.

**References**
>10

**Contact**
oleo@airliquide.com
Air Liquide Engineering & Construction now offers its many years of engineering and operational experience to Customers through a growing range of Services.

Our goal is to be your one-stop service provider to make Customers gain full visibility over Total Cost of Ownership and optimize each process in the short and longer term.
A growing range of services developed for the plants of the group

Our offer is organized in the following categories:

**Engineering Services**
Conversions, modifications, upgrades: from conceptual and feasibility studies to project execution for the improvement of operating plants; design for third parties and validation, performance improvement programs.

**Remote Support Services**
Customer training, safety studies and recommendations, technical assistance, monitoring and diagnostics from our technology centers and front-end offices.

**On-Site Services**
Deployment of our experts to site for issue resolution, performance checks, installation of components, supervision of planned or unplanned shut-down events.

**Spare Parts Services**
Customers’ spares management, supply of parts through custom lists, safety stocks, interchangeability studies, compliance with regulations.

**Customer Service Agreements (CSA)**
To strengthen the partnership with our Customers, Air Liquide Engineering & Construction also offers its Services through tailored CSAs. These CSAs are customized and adjusted to a Customer’s specific needs of support and can include services from the above categories as well as premium Services such as dedicated technical support, definition and optimization of maintenance plans, extension of guarantees. The CSA is the ideal tool to manage the Total Cost of Ownership.

**Contact**
customer-services@airliquide.com
Air Liquide Engineering & Construction offers a full range of pre- and post-sales solutions, from feasibility studies to upgrading of operating plants for performance improvement purposes.

A typical, comprehensive project includes detailed design work, procurement, supervision of installation and restart, performance validation tests to verify the effectiveness of the implemented solutions.

Engineering Services are central to Customer Service Agreements, where regular product or process improvement options are evaluated.

**Engineering Services:**
- Revampings
- Design validation
- Debottlenecking
- Studies (Screening/Feasibility/Permitting)
- Process optimization studies
- Performance improvement programs (PIP)
- Modifications / Conversions / Upgrades
- Plant life cycle assessments and extensions
- Design for third party organizations
- Project development and cost estimates

**Case Study: Unit lifetime extension**

**Mission Oxygen plant – Europe -2013:**

Our Customer wanted to revamp their plant to bring it up date and extend its life.

**Intervention:**

We identified the need to replace:
- Front end purification
- Electrical room
- Main heat exchanger of the cold box

Revamping planned to take place during planned shutdown.
We supervised the re-start of the ASU.

**Results:**

- + 15 years’ life plant
- Full compliance with more stringent safety regulations.
- Excellence of Execution
- Efficient intervention in a complex environment meeting customer requirements.

**Contact**

customer-services@airliquide.com
Remote Support Services: monitoring and analyses for prompt assistance

Air Liquide Engineering & Construction specialists can perform plant data analysis, carried out in our product/process centers of excellence to provide reliable, effective solutions using on-line, connectivity-based services. Remotely conducted predictive analyses support:

- Prevention of potential incidents or problems;
- Avoidance of costly unplanned downtime;
- Life extension programs through plant obsolescence management

To further assist operations, members of our Remote Support Services team are available to hold customized training courses for your personnel on safety, equipment, processes, operations and maintenance (O&M).

Remote Support Services:

- Plant diagnoses
- Vulnerability studies
- Accident risk analyses
- Energy efficiency assessments
- Remote monitoring and diagnostic reports
- Customer training (O&M, HSE) and upgrades
- Health, Safety and Environment (HSE) studies
- Operations and maintenance optimization studies

Contact
customer-services@airliquide.com

Case Study: Process optimization

Mission LNG Terminal, UK:

The needs of our client have changed. He wanted advice to re-optimize.

Intervention:

Experts mobilized in order to fully audit their processes:

- Detailed diagnostic with recommendations for plant optimizations in the short and long term
- Combination of Remote On-Site Support with back office analysis

Results:

- Significant reduction of OPEX:
  Optimization of common header system 30% energy reduction, Payback < 6 months
- Improved equipment lifetime
- Reduced stop and go operation of units
On-Site Services: expertise in assessments, operations, repairs

Our experienced field service engineers, the same as deployed at Air Liquide Group facilities, are at Customer’s disposal for site interventions, troubleshooting and fixes. Prompt dispatch of experts is also provided to root cause incidents and restart reliable operations after unplanned shutdown events. On-Site repair activities, executed by our qualified team, will ensure reliable plant operations for the long term to follow.

On-Site Services:

- Repairs
- Troubleshooting and fixes
- Support upon emergency call
- Performance / Efficiency checks
- Supervision for:
  - Plant operations
  - Supplier interventions
  - Planned maintenance events
  - Installation, commissioning, start-up
- Execution of plant relocation activities

Case Study: ASU relocation and uprating project to meet higher production demand

Mission ASU – Asia - 2010:

A customer asked us to plan and complete the ASU relocation, and propose a solution to increase significantly gaseous nitrogen production.

Intervention:

To address the uprating, we provided our Customer with two detailed proposals for increasing production: adding a new ASU or upgrading an existing unit. Our Customer opted for the upgrade.

Results:

- Flexible approach to evolving needs
  Our well-structured proposals and sound technical support enabled our Customer to make a well-informed decision with confidence.
- Cost-effective major production increase
  Upgrading was the best solution, in CAPEX terms, while our efficient execution made for reliability and a doubling of N₂ production.

Contact

customer-services@airliquide.com
Spare Parts Services: competent support from our supply chain

Thanks to strong relationships with selected suppliers, our E&C specialists will support you at best with custom spare part lists, specifying everything needed to respect fit, form and function of installed parts. We insure interchangeability and offer assistance related to change of suppliers, obsolescence and upgrading of parts and provide assistance in case of certification requirements to comply with the latest regulations and local jurisdictions. We also carry our consultative studies on safety and capital stocks needed to maximize the availability of your plant.

**Spare Parts Services:**
- Standard supply
- Emergency supply
- Site inventory audits
- Spare parts installation
- Safety and capital stocks
- Inspection and expediting
- Interchangeability studies
- Storage recommendations
- Obsolescence management
- Compliance with updated regulations
- Lists for planned and unplanned maintenance

**Case Study: Sourcing and procurement of an update for a 30-year-old bundle**

**Mission Chemical plant – South Africa – 2015:**
Our client had to change three 30+ years old bundles in order to increase plant’s reliability and comply with local regulations. They had no equipment documentation and the equipment was tailor made.

**Intervention:**
As the initial manufacturer didn’t exist anymore, we searched for vendors able to manufacture the bundles based on the technical documents from our archives. Several components had to be upgraded so as to comply with current local regulations. Finally, the ready to install equipment was handed to the client’s transporter together with the requested documents to apply for local certifications.

**Results:**
- Ready to install: the bundles were made to fit the plant’s design
- Performance consistency: a 12 months’ performance guarantee of the equipment

**Contact**
customer-services@airliquide.com
Customer Service Agreements (CSA): Easy ongoing access to our broad range of services and expertise

Customer Service Agreements (CSA) are the most comprehensive way to benefit from our Customer Services.

By simplifying your access to the expertise of Air Liquide, a CSA makes for a close partnership between your team and ours. This includes regular on-site meetings.

A single CSA provides you with the ongoing support of as many of our Customer Service as you require, enabling you to optimize plant performance and maximize cost control over time.

The CSA can be customized to fit your specific needs and circumstances, with options to renew or modify the subscribed services. The duration of the agreement is variable, keeping up with your requirements.

**Customer Service Agreements:**

- Easy and effective access to Air Liquide specialists and expertise:
  - Single renewable contract
  - Single contact person
  - First reply guaranteed timing
  - Practical answers with clear and easy operating instructions
  - Regular on-site meetings
- Maintenance programs
- Continuous technical support
- Extended performance guarantees
- Customer tailored terms on any selected Service

**Contact**

customer-services@airliquide.com

**Mission ASU plants – Middle East - 2017:**

Our customer wanted to increase its production, optimize the related energy consumption and sustain a good knowledge of its units.

**Intervention:**

We first assessed the current status of the units and their energy consumption:

- Off-site preparation and information gathering
- On-site visual inspection and report-out

**Results:**

A long term Service Agreement has been signed including 'on demand' specific diagnostics (feasibility studies, risk analysis, remote troubleshooting, ...), site services, spare parts services, guaranteeing the customer the best follow-up and ensuring him with support whenever requested.
How to reach us

AIR GASES  
<airgases@airliquide.com>

RARE GASES  
<raregases@airliquide.com>

CO₂ CAPTURE  
<cryocap@airliquide.com>

HYDROGEN & SYNGAS GENERATION  
<hydrogen-syngas@airliquide.com>

HYDROGEN & SYNGAS SEPARATION  
<hydrogen-syngas@airliquide.com>

CHEMICALS  
<chemicals@airliquide.com>

NATURAL GAS TREATMENT  
<gas-treatment@airliquide.com>

SULFUR  
<sulfur@airliquide.com>

LNG  
<lng@airliquide.com>

OLEOChemicalS  
<oleo@airliquide.com>

CUSTOMER SERVICES  
<customer-services@airliquide.com>

Our other locations' contact information can be found at  
www.engineering-airliquide.com
Africa
Air Liquide Engineering & Construction, South Africa
Stoneridge Office Park, 1st Floor Block E, 8 Greenstone Place
Greenstone 1609, Johannesburg
+27 87 288 1440 Email: africa.engineering@airliquide.com

Americas
Air Liquide Engineering & Construction, USA
9811 Katy Freeway, Suite 100
Houston TX 77024
Tel: +1 713 624 80 03 Email: americas.engineering@airliquide.com

Asia
Air Liquide Engineering & Construction, China
A3, Cao He Jing Modern Service High-Tech Park
No. 1528 Gu Mei Road Shanghai 200233
Tel: +86 21 60 91 90 00 Email: asia.engineering@airliquide.com

Europe
Air Liquide Engineering & Construction, France
57 avenue Carnot, BP 313
94503 Champigny-sur-Marne
Tel: +33 1 49 83 55 55 Email: europe.engineering@airliquide.com
Air Liquide Engineering & Construction, Germany
Olof-Palme-Str. 35
60439 Frankfurt am Main
Tel: +49 69 580 80 Email: europe.engineering@airliquide.com

India
Air Liquide Engineering & Construction, India
A24/10 Mohan Cooperative
Industrial Estate Mathura Road Delhi 110 044
Tel: +91 11 42 59 50 50 Email: india.engineering@airliquide.com

Middle-East
Air Liquide Engineering & Construction, United Arab Emirates
Dubai Airport Free Zone, 5 East, Block A
Suite 301, P.O. Box 54368
Dubai
Tel: +97 1 42 05 55 00 Email: middleeast.engineering@airliquide.com
## List of abbreviations and acronyms

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<thead>
<tr>
<th>Abbreviation</th>
<th>Description</th>
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<tbody>
<tr>
<td>2EHA</td>
<td>2-ethylhexylacrylate</td>
</tr>
<tr>
<td>2EHOH</td>
<td>2-ethylhexanol</td>
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<tr>
<td>AA</td>
<td>Acrylic acid</td>
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<tr>
<td>AcAc</td>
<td>Acetic acid</td>
</tr>
<tr>
<td>AGR</td>
<td>Acid gas removal</td>
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<tr>
<td>APH</td>
<td>Air pre-heater</td>
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<td>Ar</td>
<td>Argon</td>
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<tr>
<td>ASU</td>
<td>Air Separation Unit</td>
</tr>
<tr>
<td>ATR</td>
<td>Autothermal reformer/reforming</td>
</tr>
<tr>
<td>BA</td>
<td>Butylacrylate</td>
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<tr>
<td>BFD</td>
<td>Block flow diagram</td>
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<tr>
<td>BFW</td>
<td>Boiler feedwater</td>
</tr>
<tr>
<td>BOG</td>
<td>Boil-off gas</td>
</tr>
<tr>
<td>BTU</td>
<td>British thermal unit</td>
</tr>
<tr>
<td>BuOH</td>
<td>Butanol</td>
</tr>
<tr>
<td>C2+</td>
<td>Hydrocarbons with 2 or more carbons</td>
</tr>
<tr>
<td>C4</td>
<td>Mixture of 4-carbon hydrocarbons (butane, butylene and butadienes)</td>
</tr>
<tr>
<td>Capex</td>
<td>Capital expenditures</td>
</tr>
<tr>
<td>CCR</td>
<td>Continuous catalytic reforming</td>
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<td>CDU</td>
<td>Crude distillation unit</td>
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<td>CH4</td>
<td>Methane</td>
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<td>CLS</td>
<td>Claus</td>
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<td>CO</td>
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<td>CO2</td>
<td>Carbon dioxide</td>
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<tr>
<td>COS</td>
<td>Carbonyl sulfide</td>
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<td>CSFT</td>
<td>Cold soak filtration test</td>
</tr>
<tr>
<td>Cu</td>
<td>Copper</td>
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<tr>
<td>CW</td>
<td>Cooling water</td>
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<tr>
<td>DEA</td>
<td>Diethanolamine</td>
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<tr>
<td>DME</td>
<td>Dimethyl ether</td>
</tr>
<tr>
<td>DMR</td>
<td>Dehydration and mercaptan removal unit</td>
</tr>
<tr>
<td>DRI</td>
<td>Direct reduction of iron ore</td>
</tr>
<tr>
<td>DTDC</td>
<td>Desolventizer, toaster, dryer and cooler</td>
</tr>
<tr>
<td>E&amp;C</td>
<td>Engineering and construction</td>
</tr>
<tr>
<td>EA</td>
<td>Ethylacrylate</td>
</tr>
<tr>
<td>EAA</td>
<td>Ester-grade acrylic acid</td>
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<tr>
<td>EOR</td>
<td>Enhanced oil recovery</td>
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<tr>
<td>EtOH</td>
<td>Ethanol</td>
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<tr>
<td>FAD</td>
<td>Fatty acid distillate</td>
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<tr>
<td>FAME</td>
<td>Fatty acid methyl ester</td>
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<tr>
<td>FBDB</td>
<td>Fixed bed dry bottom gasifier</td>
</tr>
<tr>
<td>FEED</td>
<td>Front-end engineering design</td>
</tr>
<tr>
<td>FFA</td>
<td>Free fatty acid</td>
</tr>
<tr>
<td>FOB</td>
<td>Free on board</td>
</tr>
<tr>
<td>F-T</td>
<td>Fischer-Tropsch</td>
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<tr>
<td>G2G</td>
<td>Gas-to-Gasoline</td>
</tr>
<tr>
<td>GAN</td>
<td>Gaseous nitrogen</td>
</tr>
<tr>
<td>GAR</td>
<td>Gaseous argon</td>
</tr>
<tr>
<td>GNG</td>
<td>Gaseous natural gas</td>
</tr>
<tr>
<td>GOX</td>
<td>Gaseous oxygen</td>
</tr>
<tr>
<td>H2</td>
<td>Hydrogen</td>
</tr>
<tr>
<td>H2S</td>
<td>Hydrogen sulfide</td>
</tr>
<tr>
<td>HC</td>
<td>Hydrocarbon</td>
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<tr>
<td>HCl</td>
<td>Hydrochloric acid</td>
</tr>
<tr>
<td>HCN</td>
<td>Hydrogen cyanide</td>
</tr>
<tr>
<td>HDS</td>
<td>Hydrodesulfurization</td>
</tr>
<tr>
<td>He</td>
<td>Helium</td>
</tr>
<tr>
<td>HF</td>
<td>Hydrofluoric acid</td>
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<tr>
<td>Hg</td>
<td>Mercury</td>
</tr>
<tr>
<td>HHC</td>
<td>Heavy hydrocarbon</td>
</tr>
<tr>
<td>HP</td>
<td>High pressure</td>
</tr>
<tr>
<td>HT</td>
<td>High temperature</td>
</tr>
<tr>
<td>IGCC</td>
<td>Integrated gasification combined cycle</td>
</tr>
<tr>
<td>IMPCA</td>
<td>International methanol producers and consumers association</td>
</tr>
<tr>
<td>ISO</td>
<td>International Organization for Standardization</td>
</tr>
<tr>
<td>Kr</td>
<td>Krypton</td>
</tr>
<tr>
<td>LAR</td>
<td>Liquid argon</td>
</tr>
<tr>
<td>LIN</td>
<td>Liquid nitrogen</td>
</tr>
<tr>
<td>LNG</td>
<td>Liquefied natural gas</td>
</tr>
<tr>
<td>LOX</td>
<td>Liquid oxygen</td>
</tr>
<tr>
<td>LP</td>
<td>Low pressure</td>
</tr>
<tr>
<td>LP3</td>
<td>Low pressure fatty alcohols production</td>
</tr>
<tr>
<td>LPG</td>
<td>Liquefied petroleum gas</td>
</tr>
<tr>
<td>LTGT</td>
<td>Lurgi tailgas treatment</td>
</tr>
<tr>
<td>MA</td>
<td>Methylacrylate</td>
</tr>
<tr>
<td>MDEA</td>
<td>Methyl diethanolamine</td>
</tr>
<tr>
<td>MDI</td>
<td>Methylene diphenyl disocyanate</td>
</tr>
<tr>
<td>MEA</td>
<td>Monoethanolamine</td>
</tr>
<tr>
<td>MEG</td>
<td>Monoethylene glycol</td>
</tr>
<tr>
<td>MeOH</td>
<td>Methanol</td>
</tr>
<tr>
<td>MP</td>
<td>Medium pressure</td>
</tr>
<tr>
<td>MPG</td>
<td>Multi-purpose gasifier Mono propylene glycol</td>
</tr>
<tr>
<td>MTG</td>
<td>Methanol-to-Gasoline</td>
</tr>
<tr>
<td>MTP</td>
<td>Methanol-to-Propylene</td>
</tr>
<tr>
<td>NaOH</td>
<td>Soda</td>
</tr>
<tr>
<td>Ne</td>
<td>Neon</td>
</tr>
<tr>
<td>NG</td>
<td>Natural gas</td>
</tr>
<tr>
<td>NGL</td>
<td>Natural gas liquids</td>
</tr>
<tr>
<td>NH3</td>
<td>Ammonia</td>
</tr>
<tr>
<td>Ni</td>
<td>Nickel</td>
</tr>
<tr>
<td>NMP</td>
<td>N-methy pyrrolidine</td>
</tr>
<tr>
<td>NO</td>
<td>Nitrous oxide</td>
</tr>
<tr>
<td>NOx</td>
<td>Nitrous oxides</td>
</tr>
<tr>
<td>NRU</td>
<td>Nitrogen removal unit</td>
</tr>
<tr>
<td>Opex</td>
<td>Operating expenditures</td>
</tr>
<tr>
<td>PAH</td>
<td>Polycyclic aromatic hydrocarbon</td>
</tr>
<tr>
<td>PC</td>
<td>Polycarbonate</td>
</tr>
<tr>
<td>PDH</td>
<td>Propane dehydrogenation</td>
</tr>
<tr>
<td>PDP</td>
<td>Preliminary design package</td>
</tr>
<tr>
<td>PIMS</td>
<td>Proprietary simulation software</td>
</tr>
<tr>
<td>PIP</td>
<td>Performance improvement program</td>
</tr>
<tr>
<td>POX</td>
<td>Partial oxidation</td>
</tr>
<tr>
<td>PSA</td>
<td>Pressure swing adsorption</td>
</tr>
<tr>
<td>PSD</td>
<td>Prevention of significant deterioration</td>
</tr>
<tr>
<td>PTSA</td>
<td>Para-toluene sulfuric acid</td>
</tr>
<tr>
<td>RBD</td>
<td>Refined, bleached and deodorized</td>
</tr>
<tr>
<td>RSH</td>
<td>Carbon-bonded sulfhydryl or thiol</td>
</tr>
<tr>
<td>SMR</td>
<td>Steam methane reforming or reformer</td>
</tr>
<tr>
<td>SNG</td>
<td>Synthetic natural gas</td>
</tr>
<tr>
<td>SO2</td>
<td>Sulfur dioxide</td>
</tr>
<tr>
<td>SOx</td>
<td>Sulfur oxides</td>
</tr>
<tr>
<td>SRU</td>
<td>Sulfur removal unit</td>
</tr>
<tr>
<td>TDI</td>
<td>Toluene diisocyanate</td>
</tr>
<tr>
<td>USD</td>
<td>United States dollar</td>
</tr>
<tr>
<td>VDU</td>
<td>Vacuum distillation unit</td>
</tr>
<tr>
<td>VSA</td>
<td>Vacuum Swing Adsorption</td>
</tr>
<tr>
<td>WHRS</td>
<td>Waste heat recovery system</td>
</tr>
<tr>
<td>Xe</td>
<td>Xenon</td>
</tr>
</tbody>
</table>
Allows users to quickly access a host of information on the physical and chemical properties of 64 gas molecules (oxygen, nitrogen, hydrogen, etc.) in their solid, liquid and gaseous states.

Gives users the ability to instantly calculate volume conversions from gaseous to liquid state for 14 gas molecules such as nitrogen, oxygen and hydrogen.

Available on Google Play and Appstore

This manual is also available in:

DIGITAL VERSION
Send request to any email address on pages 102/103 or any Air Liquide Engineering & Construction representative

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EASY GAS CONVERTER
GAS ENCYCLOPEDIA
https://encyclopedia.airliquide.com

GAS ENCYCLOPEDIA
Allows users to quickly access a host of information on the physical and chemical properties of 64 gas molecules (oxygen, nitrogen, hydrogen, etc.) in their solid, liquid and gaseous states.
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Economic hypothesis and definitions: Unless otherwise specified, Opex calculations include variable operating costs (utilities, feedstock…) and fixed costs (labour…). Natural gas cost is assumed to be $4/mmBTU HHV. In addition, unless otherwise specified, Capex is calculated either: a) including all EPC costs (process units, offsite and utilities) but excluding owner’s costs for a plant built on the USGC; or, b) using 1.8xEP costs (process units, offsite and utilities). Price base is 2017. Opex and Capex are indicative and can vary according to the basis of design, such as: product(s) yield and quality, site conditions, feedstock quality, utilities, project scope and plant capacity. Units are metric. Gallons (gal) are US Gallons (3.785 liters). Barrel (bbl) refers to oil barrel (42 gal). Heating value shall be understood as Lower Heating Value (LHV). Exchange rate used is: 1 Euro = 1.1 US Dollar.

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Contact information for suggestions, improvements… email at EditorTH@airliquide.com

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